

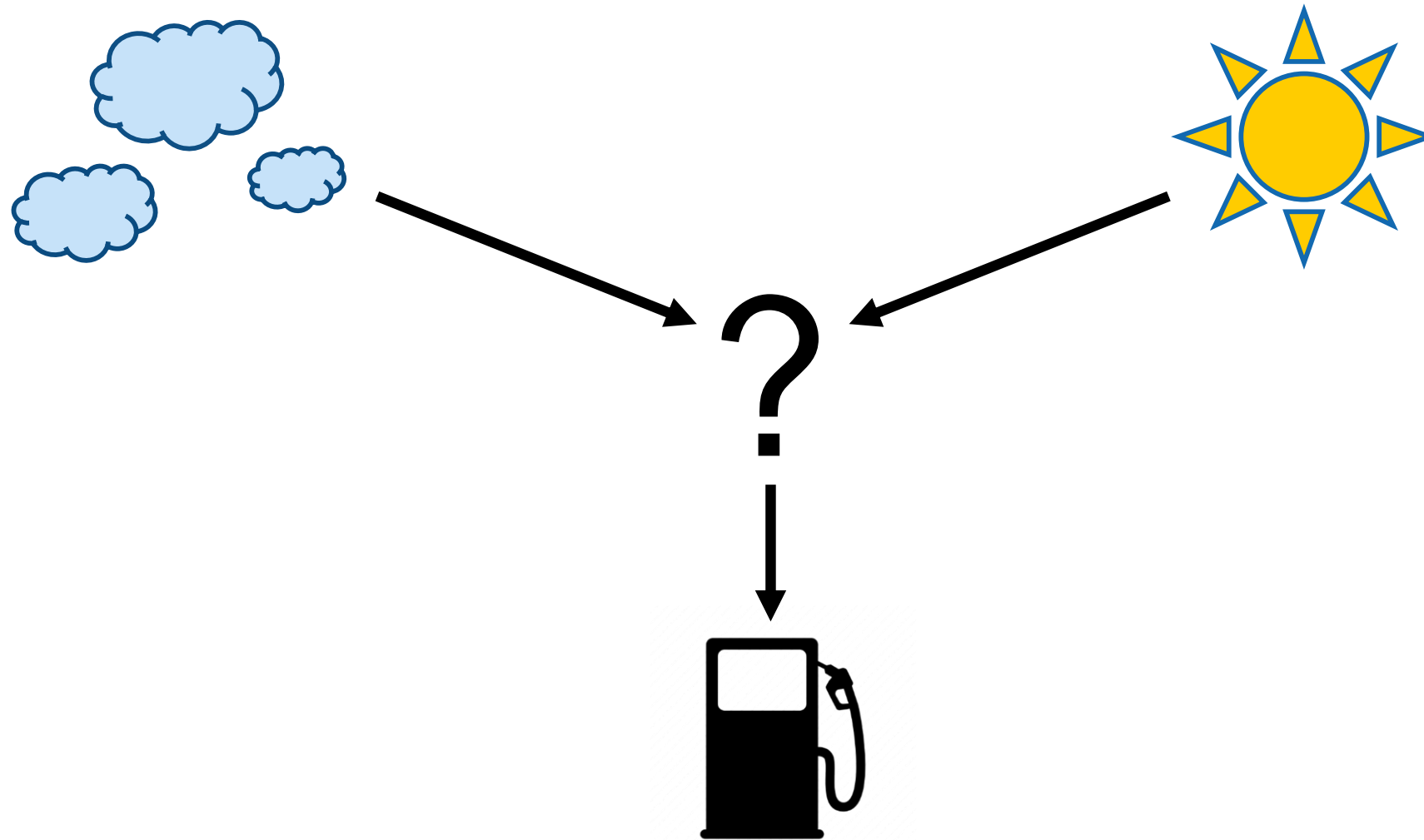


Fuel from Sunlight and Air – Demonstration of the Thermochemical Pathway

Remo Schäppi, Aldo Steinfeld
Professorship of Renewable Energy Carriers, ETH Zürich

LTP/PSI Thursday Colloquia, October 2022, PSI, Villigen

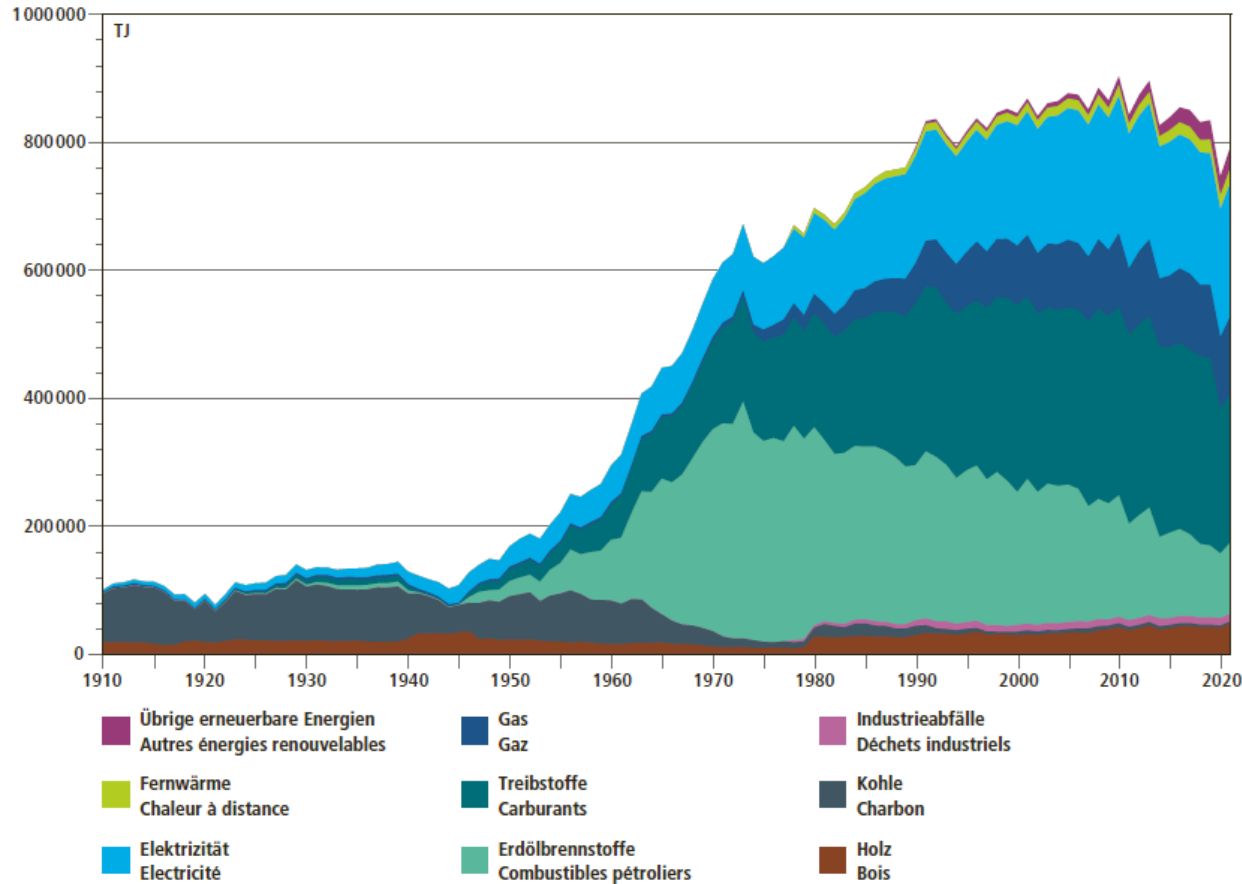
Fuel production from sunlight and air



Energy consumption in Switzerland

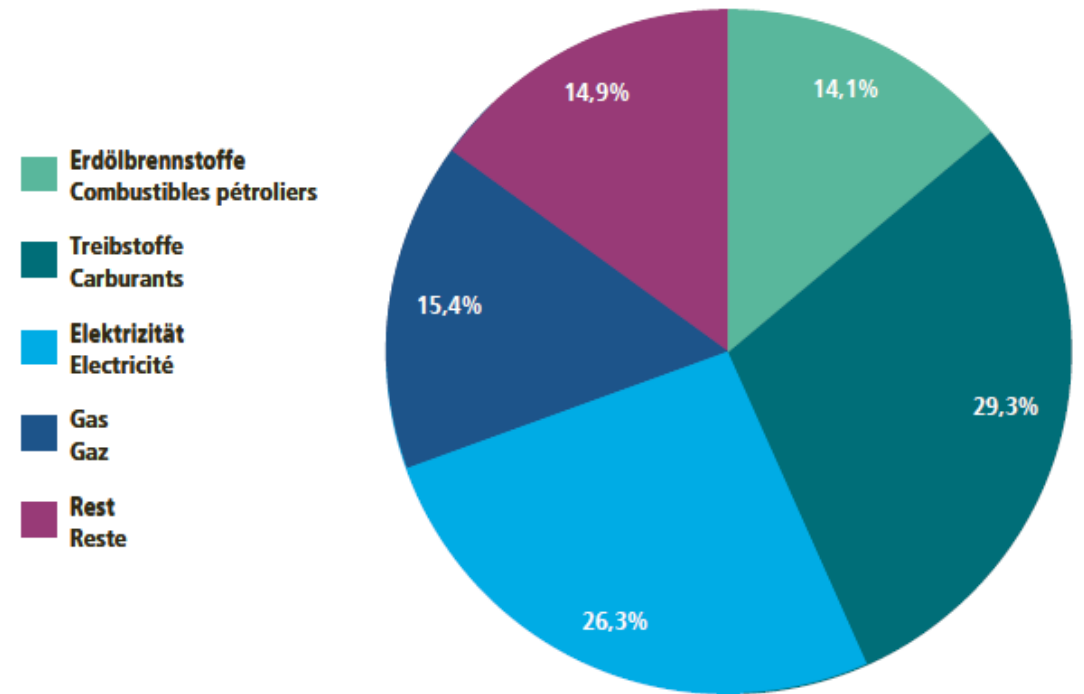
Total final consumption by source

Fig. 1 Endenergieverbrauch 1910–2021 nach Energieträgern
Consommation finale 1910–2021 selon les agents énergétiques



BFE, Schweizerische Gesamtenergiestatistik 2021 (Fig. 1)
OFEN, Statistique globale suisse de l'énergie 2021 (fig. 1)

Fig. 2 Aufteilung des Endverbrauchs nach Energieträgern (2021)
Répartition de la consommation finale selon les agents énergétiques (2021)

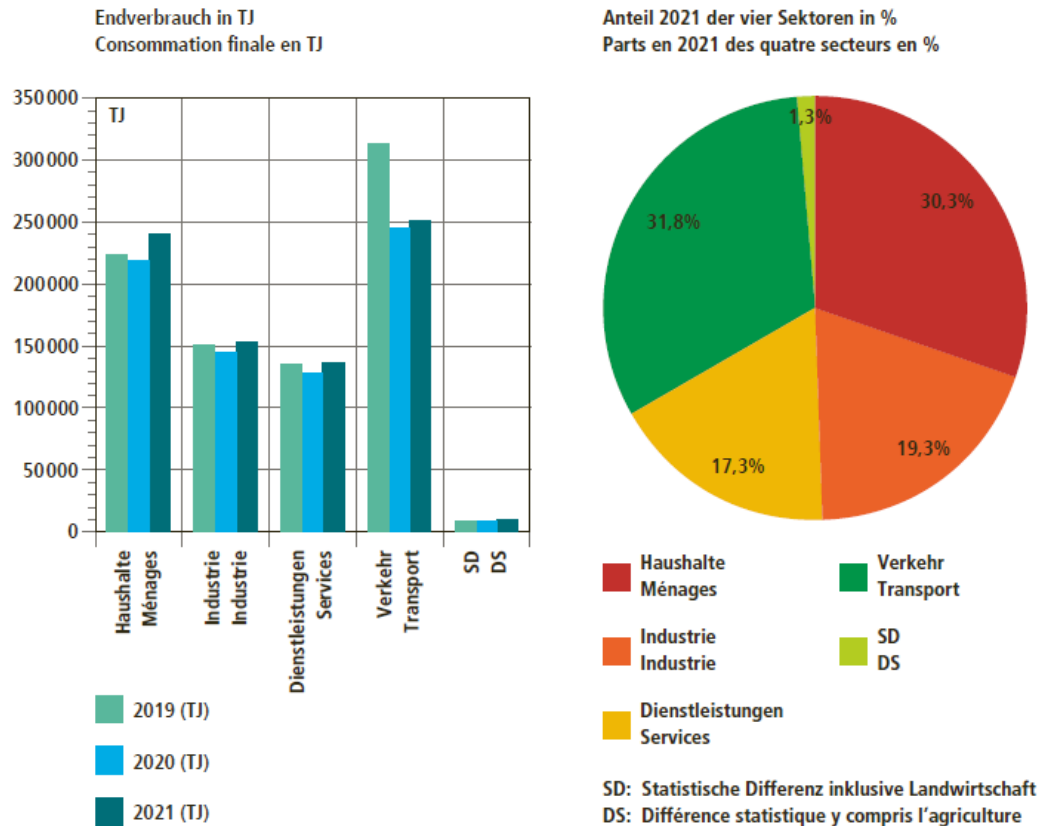


BFE, Schweizerische Gesamtenergiestatistik 2021 (Fig. 2)
OFEN, Statistique globale suisse de l'énergie 2021 (fig. 2)

Energy consumption in Switzerland

Total final consumption by sector

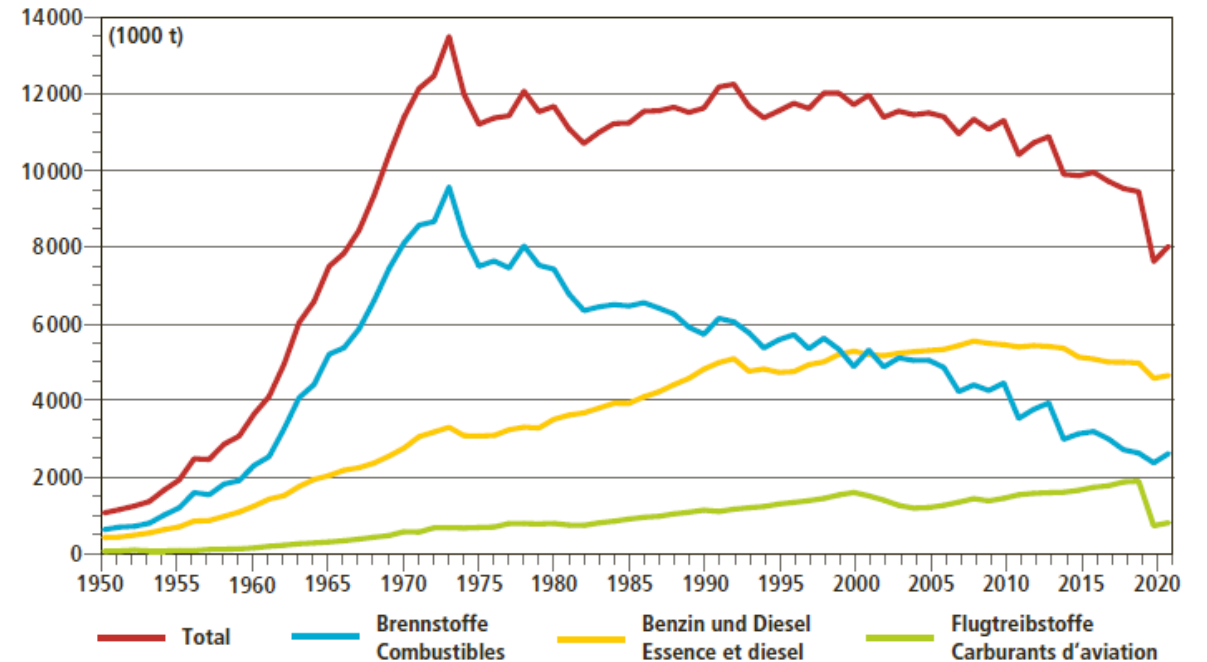
Fig. 3 Aufteilung des Energie-Endverbrauchs nach Verbrauchergruppen
Répartition de la consommation finale d'énergie selon les groupes de consommateurs



BFE, Schweizerische Gesamtenergiestatistik 2021 (Fig. 3)
OFEN, Statistique globale suisse de l'énergie 2021 (fig. 3)

Final consumption of oil products

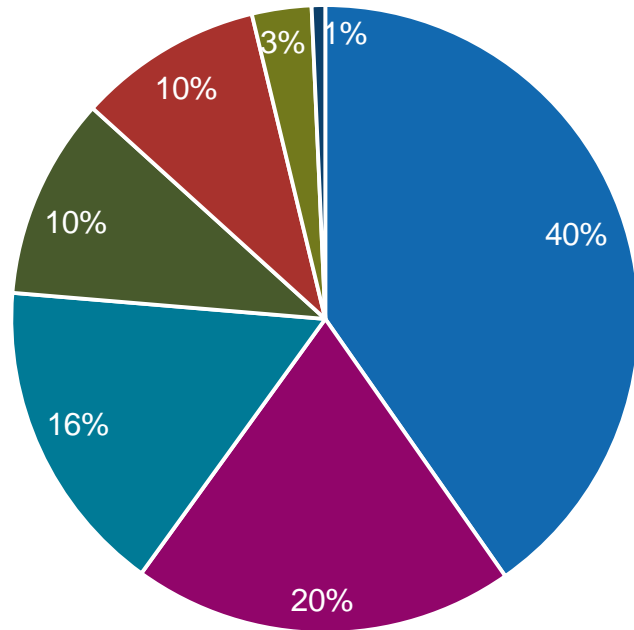
Fig. 10 Entwicklung des Endverbrauchs der Erdölprodukte
Evolution de la consommation finale des produits pétroliers



BFE, Schweizerische Gesamtenergiestatistik 2021 (Fig. 10)
OFEN, Statistique globale suisse de l'énergie 2021 (fig. 10)

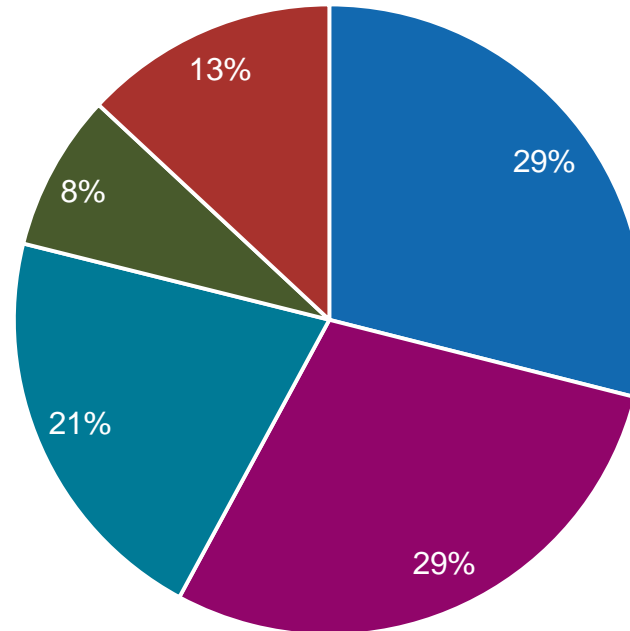
World energy consumption and supply (418 EJ)

Total final consumption by source



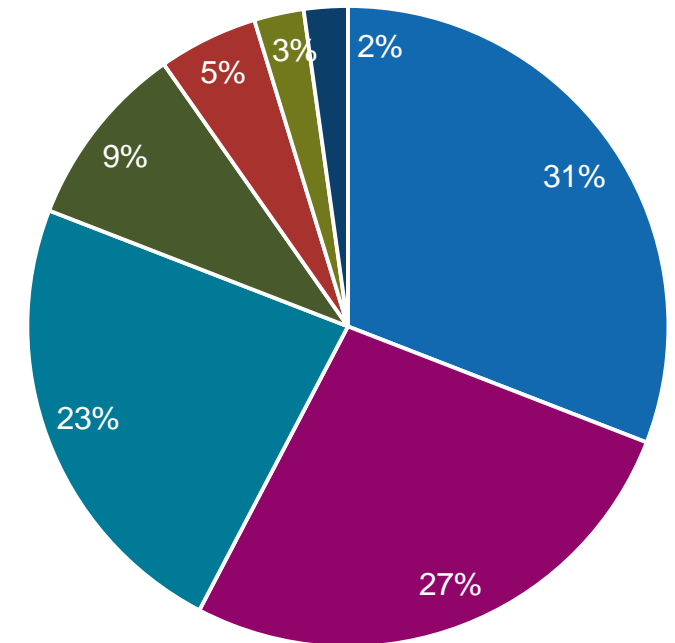
- Oil products
- Electricity
- Natural gas
- Bioufuels & waste
- Coal
- Heat
- Rest

Total final consumption by sector



- Transport
- Industry
- Residential
- Services
- Rest

Total energy supply by source



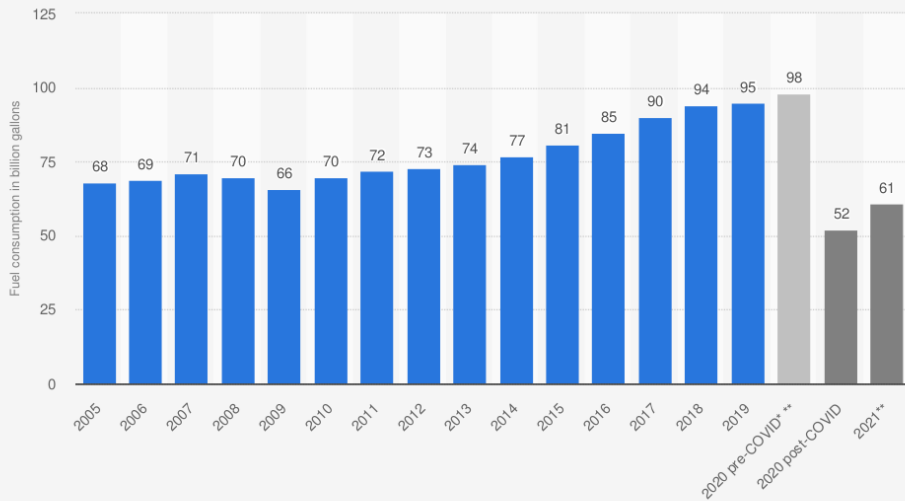
- Oil
- Coal
- Natural gas
- Bioufuels & waste
- Nuclear
- Hydro
- Wind, Solar, etc.

Quelle: IEA, 2019

Aviation fuel use and CO₂ emissions

- ~2-2.5% of total anthropogenic CO₂ emissions
- ~12% of CO₂ emissions from transport sources

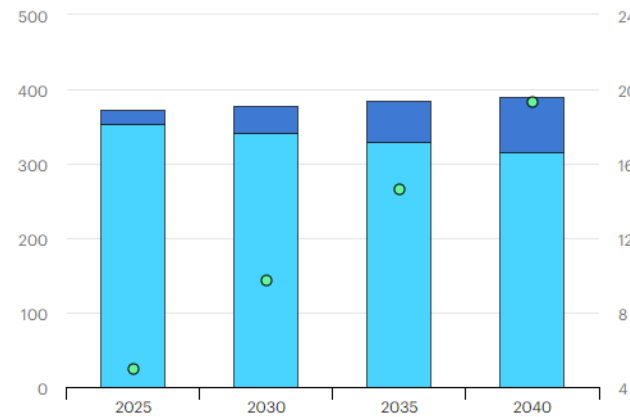
Total fuel consumption of commercial airlines worldwide between 2005 and 2021 (in billion gallons)



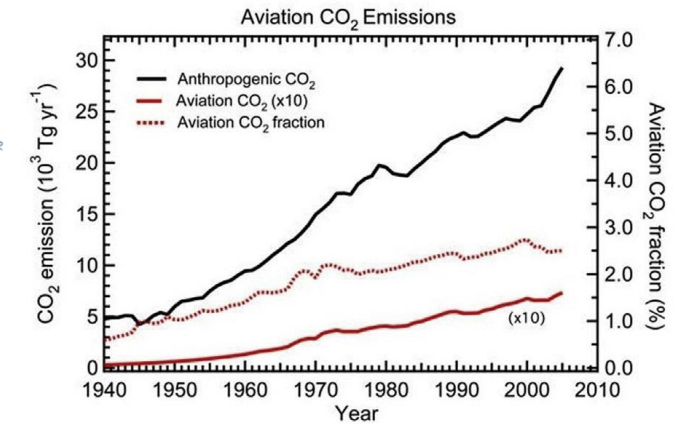
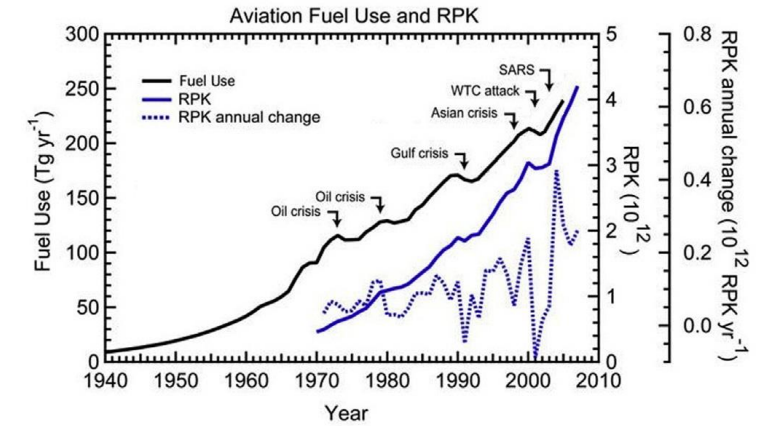
Sources
IATA; ICAO
© Statista 2021

Additional Information:
Worldwide; IATA; ICAO; 2005 to 2020

Aviation fuel consumption in the Sustainable Development Scenario, 2025-2040

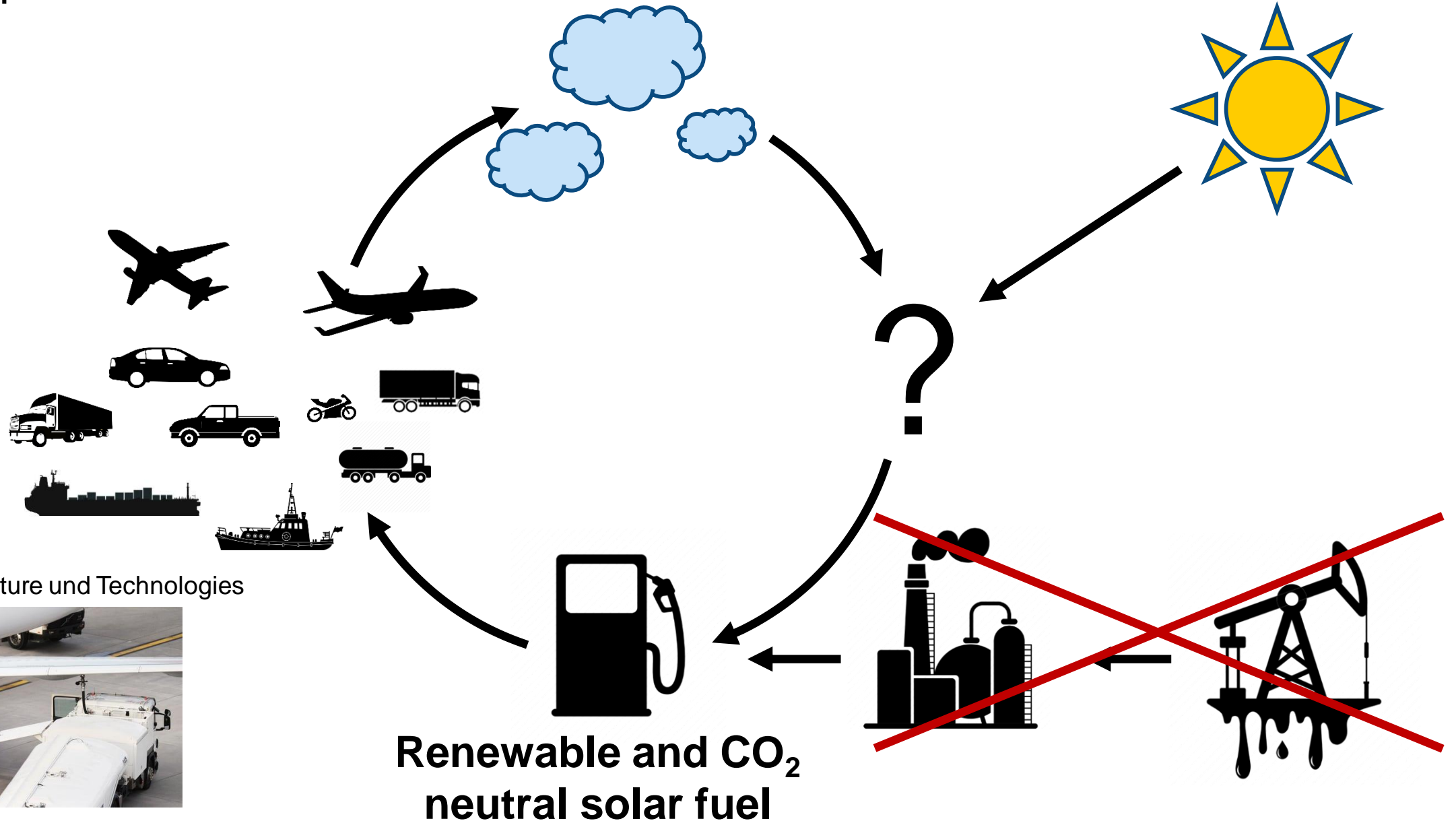


● Fossil jet kerosene ● SAF ● Share of SAF (right-axis)

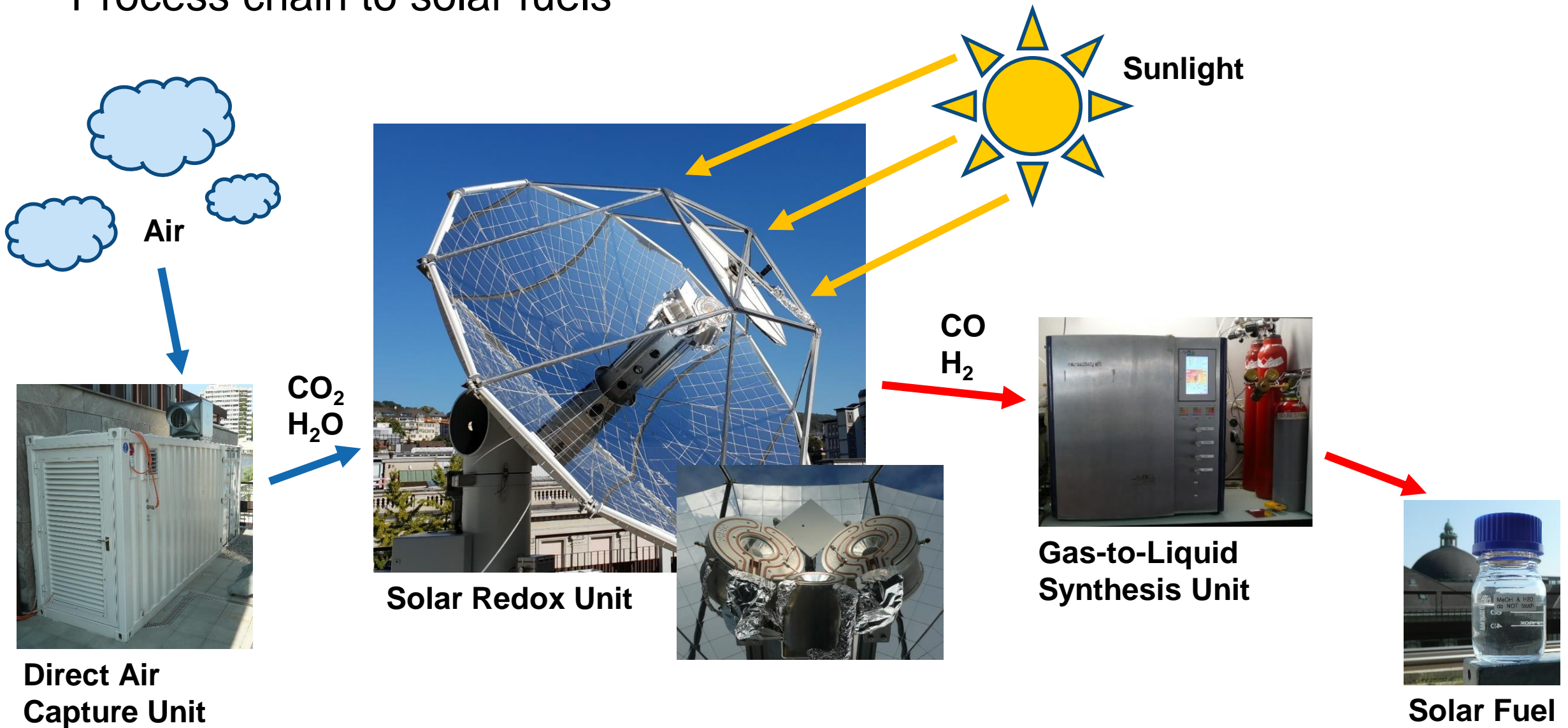


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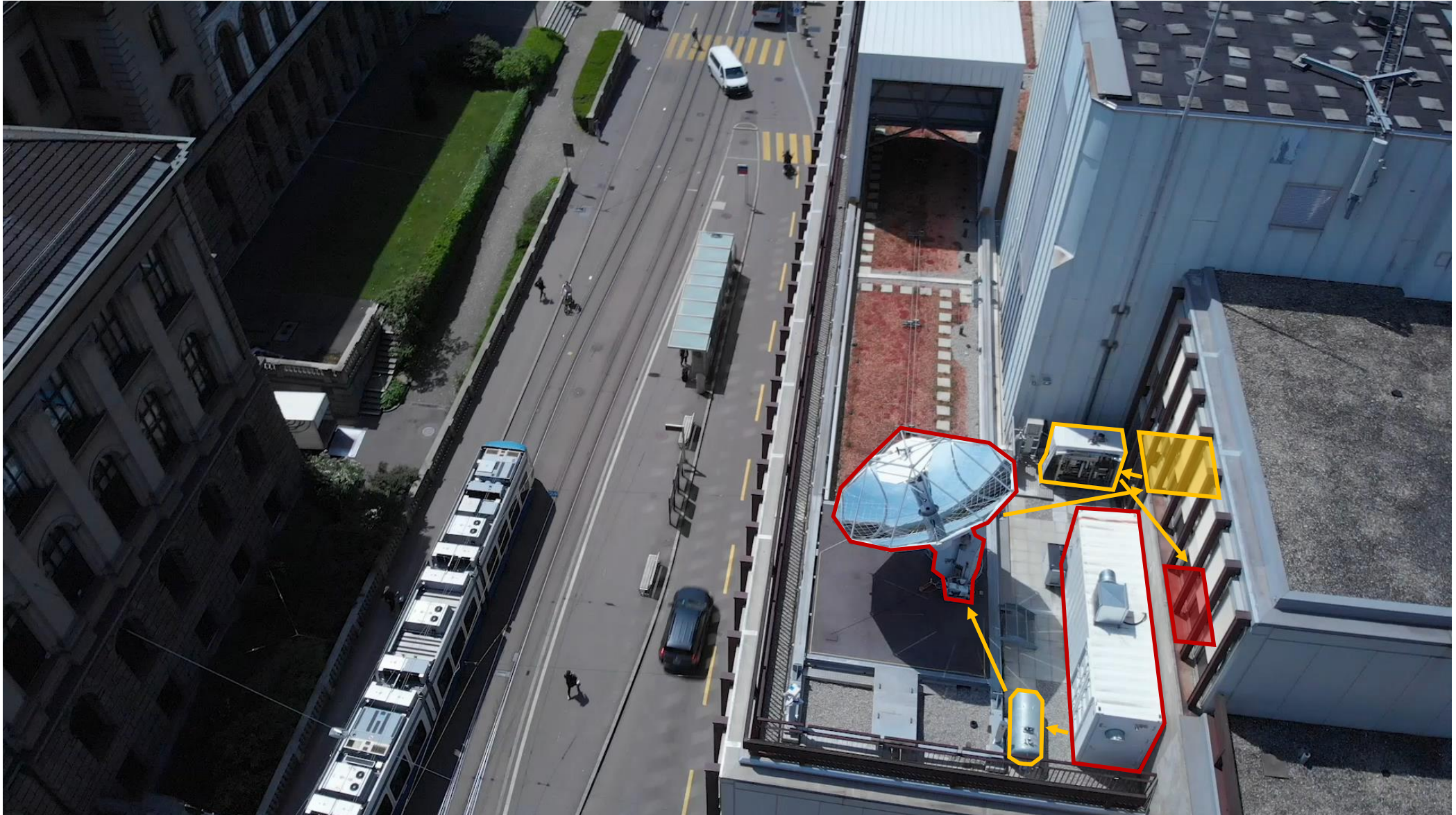
Fuel production



Process chain to solar fuels

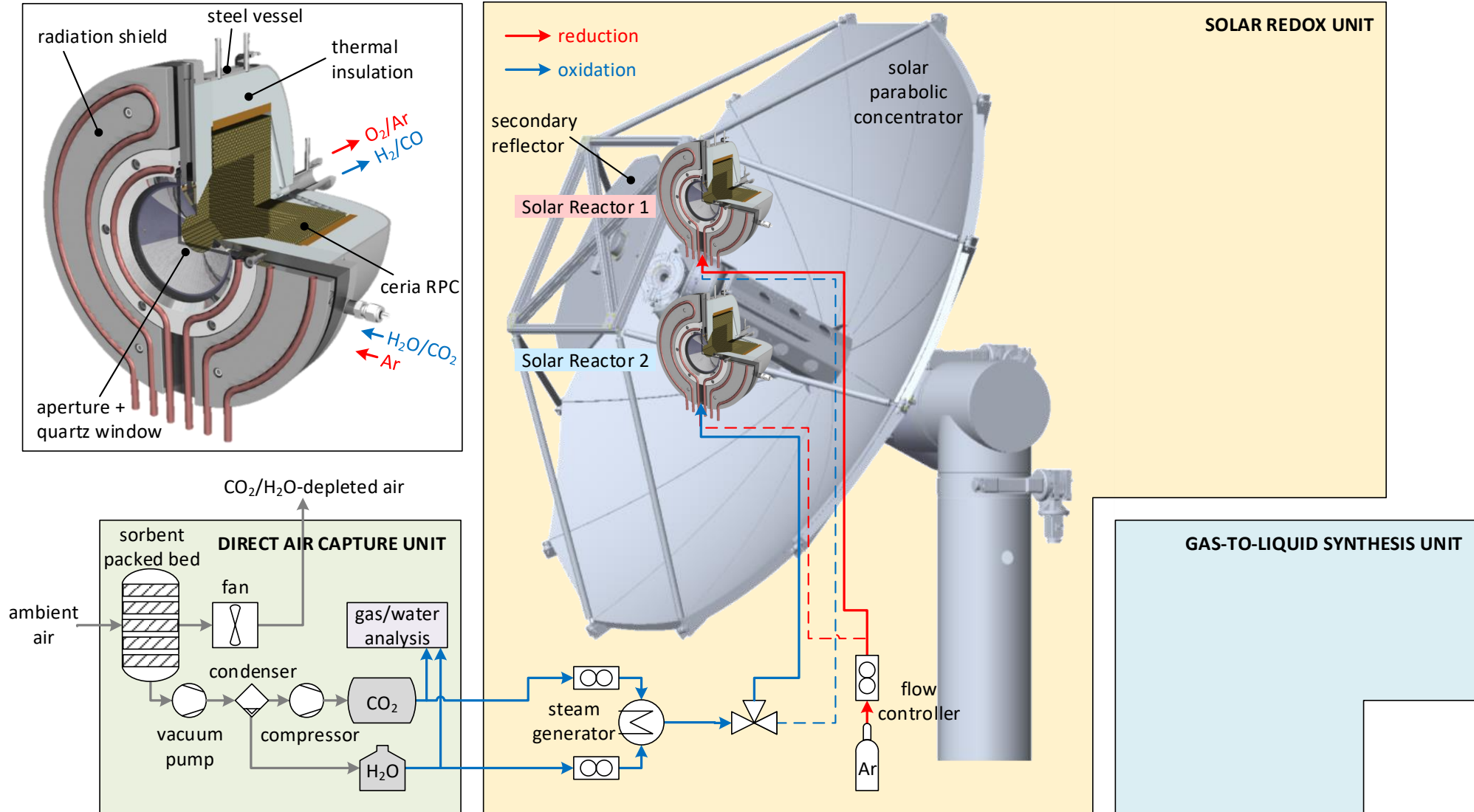


Setup on the roof of ETH machine laboratory in Zürich



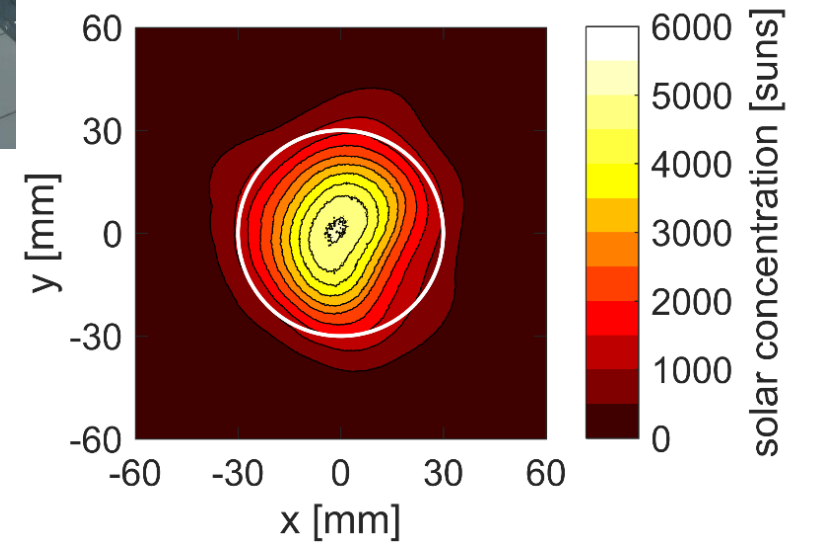
© ETH Zürich / Alessandro Della Bella

Schematic of the implemented process chain



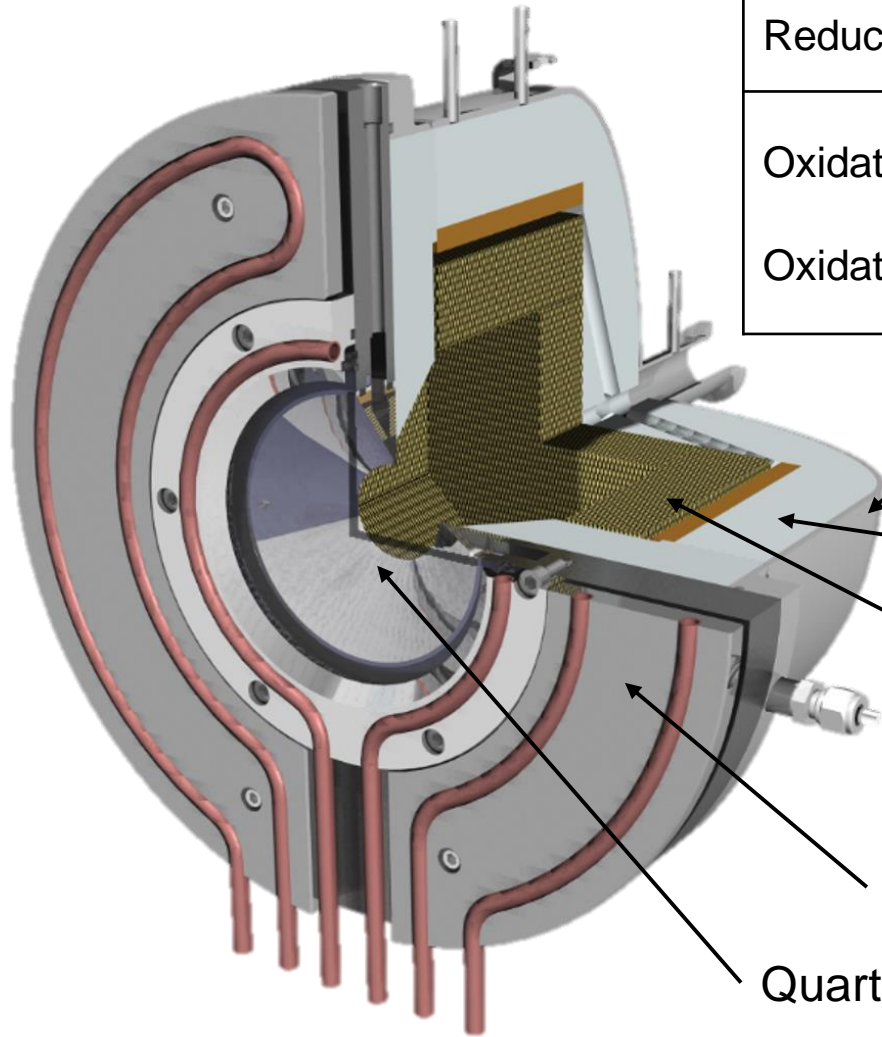
Source: Schäppi, R. *et al.* Drop-in Fuels from Sunlight and Air. *Nature* (2021).

Solar Redox Unit

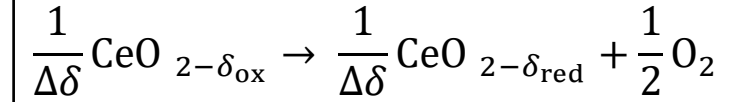


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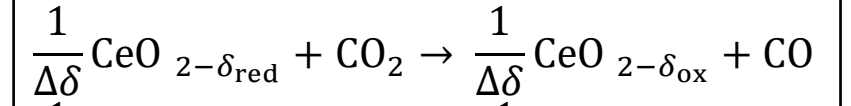
Solar Reactors



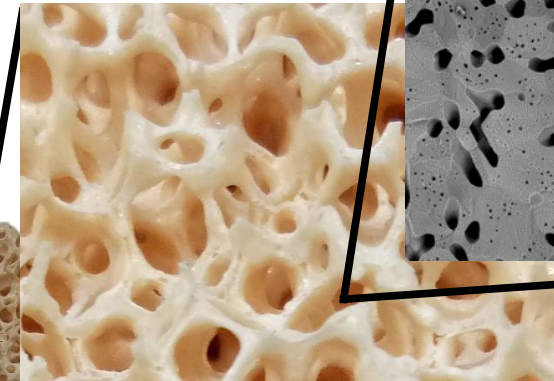
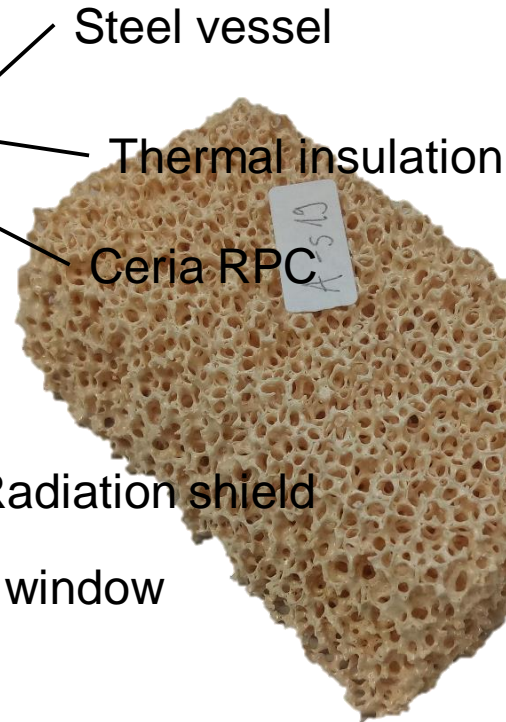
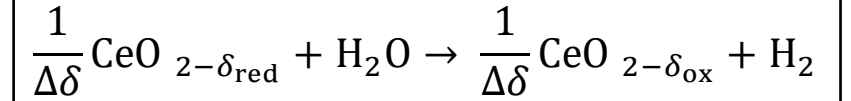
Reduction: $\Delta H \approx 475$ kJ per $\frac{1}{2}$ mole O_2



Oxidation with CO_2 : $\Delta H \approx -192$ kJ/mol CO_2



Oxidation with H_2O : $\Delta H \approx -234$ kJ/mol H_2

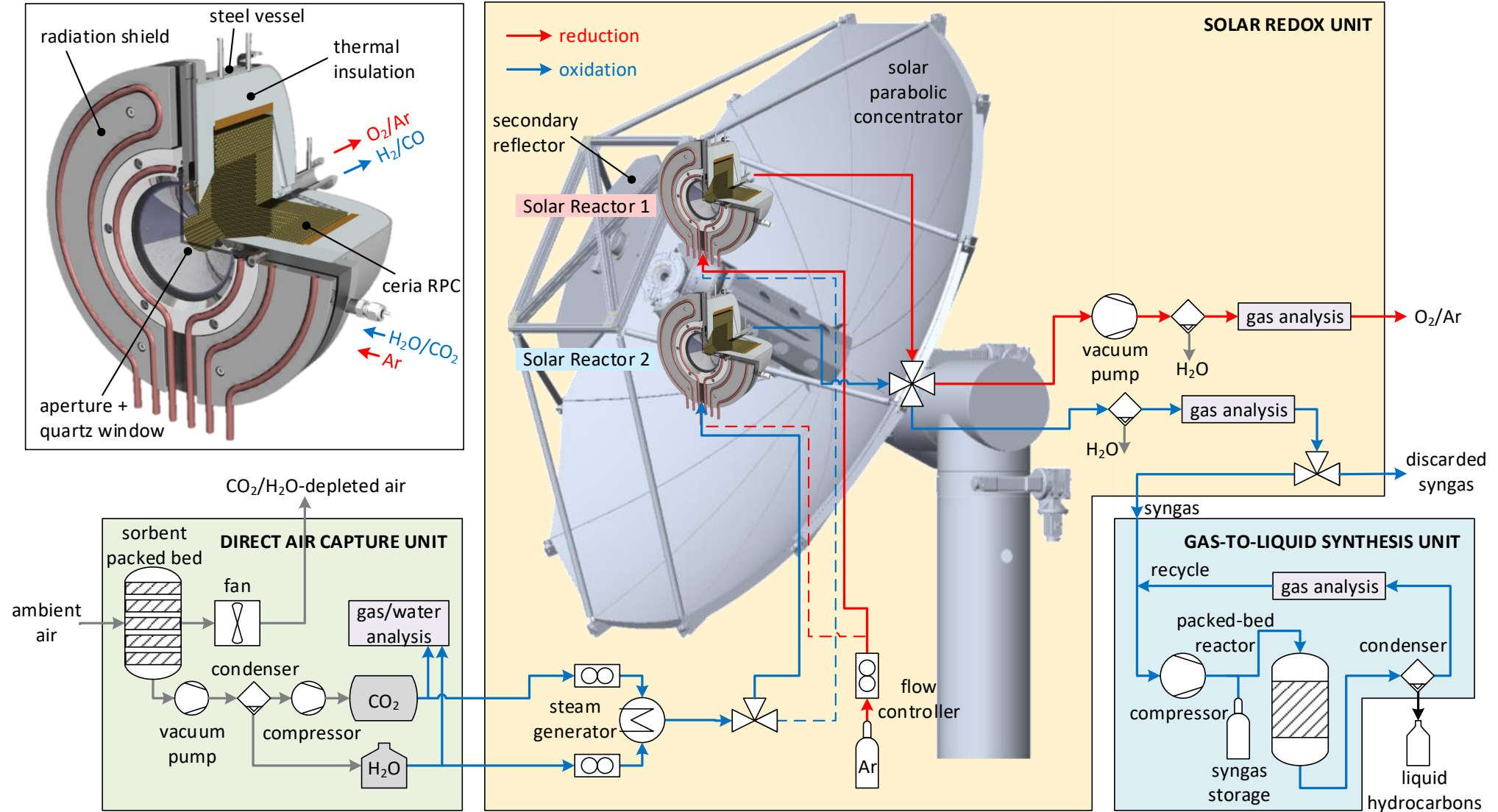


10 mm



100 μm

Schematic of the implemented process chain



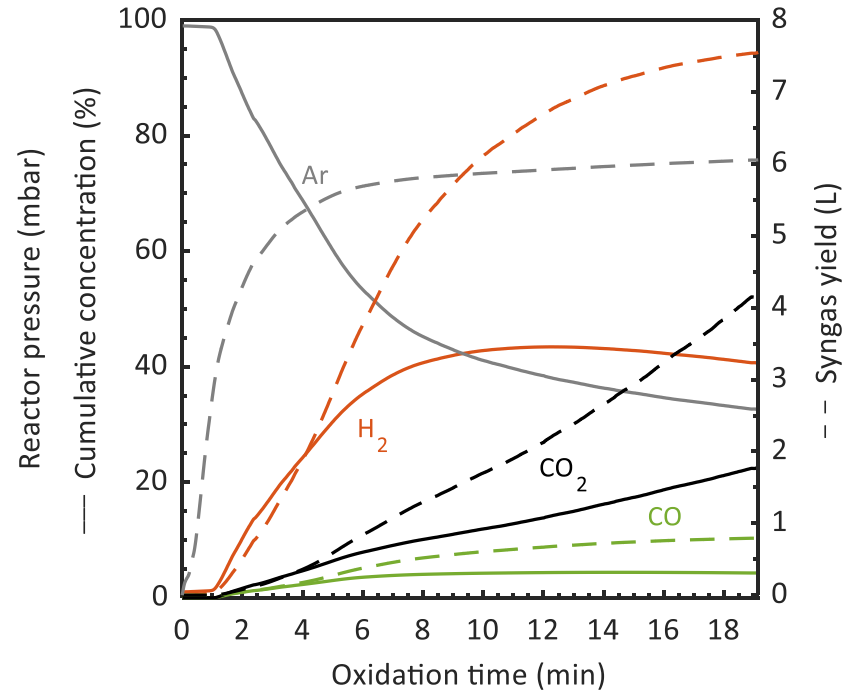
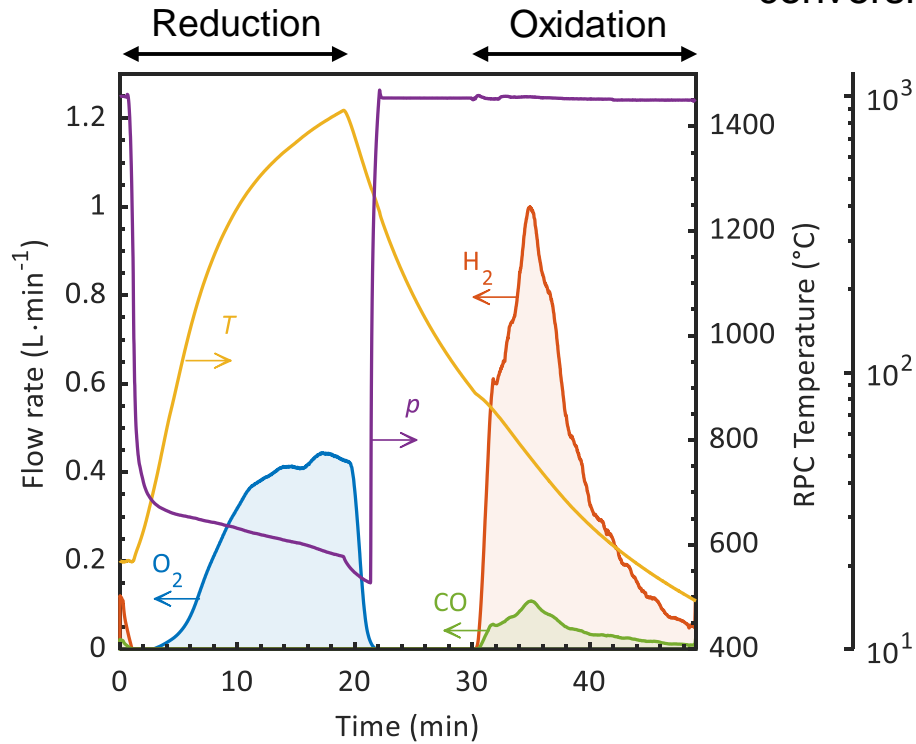
Source: Schäppi, R. et al. Drop-in Fuels from Sunlight and Air. *Nature* (2021).

Exemplary Cycle Targeting Syngas for Methanol Synthesis

Target:

H_2/CO_x ratio: 2 – 3

Depending on catalyst and CO_2 conversion



- Full oxidation:
 - 18.5 L of syngas
 - 40.7% H_2 , 4.3% CO, 22.4% CO_2 , 32.6% Ar
 - H_2/CO_x ratio: 1.52
 - CO_2 conversion: 16.1%

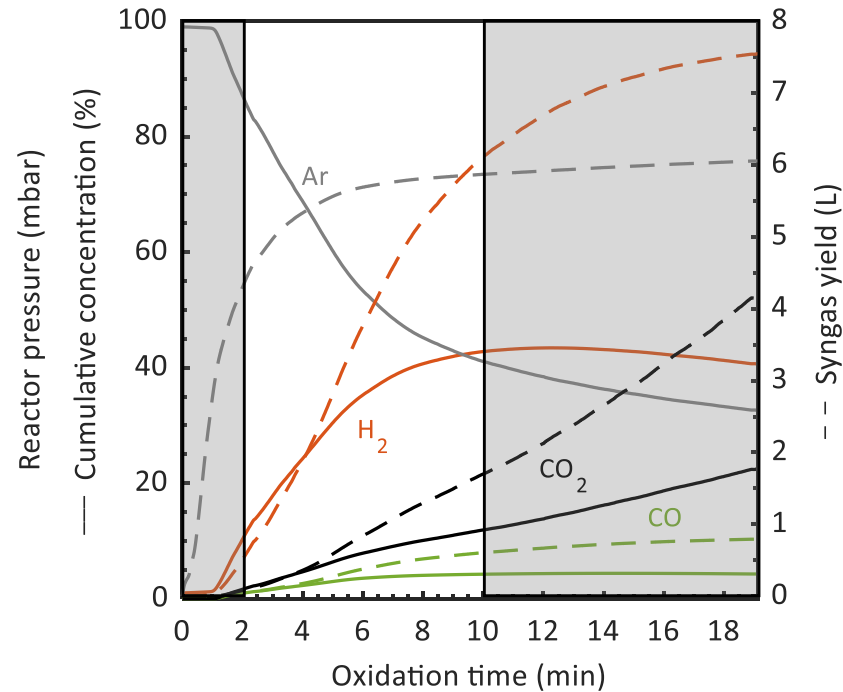
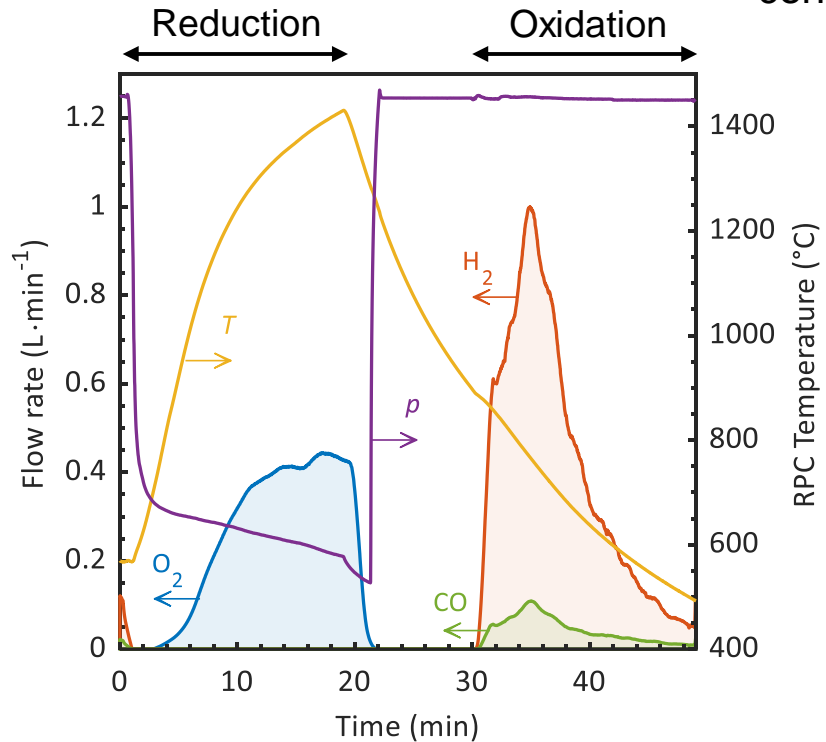
Conditions	Reduction	Oxidation
Power input	5.1 kW	Off-sun (0 kW)
Gas flow	0.5 l/min Ar	0.4 l/min CO_2 9.8 g/min H_2O
Pressure	25 mbar	1 bar

Exemplary Cycle Targeting Syngas for Methanol Synthesis

Target:

H_2/CO_x ratio: 2 – 3

Depending on catalyst and CO_2 conversion



- 0 - 2 min:
 - 4.9 L of syngas
 - 10.2% H_2 , 0.9% CO , 1.6% CO_2 , 87.3% Ar
 - H_2/CO_x ratio: 4
 - CO_2 conversion: 36%
- 10 min - full oxidation:
 - 4.2 L of syngas
 - 33.6% H_2 , 4.5% CO , 57.7% CO_2 , 4.2% Ar
 - H_2/CO_x ratio: 0.54
 - CO_2 conversion: 7.2%

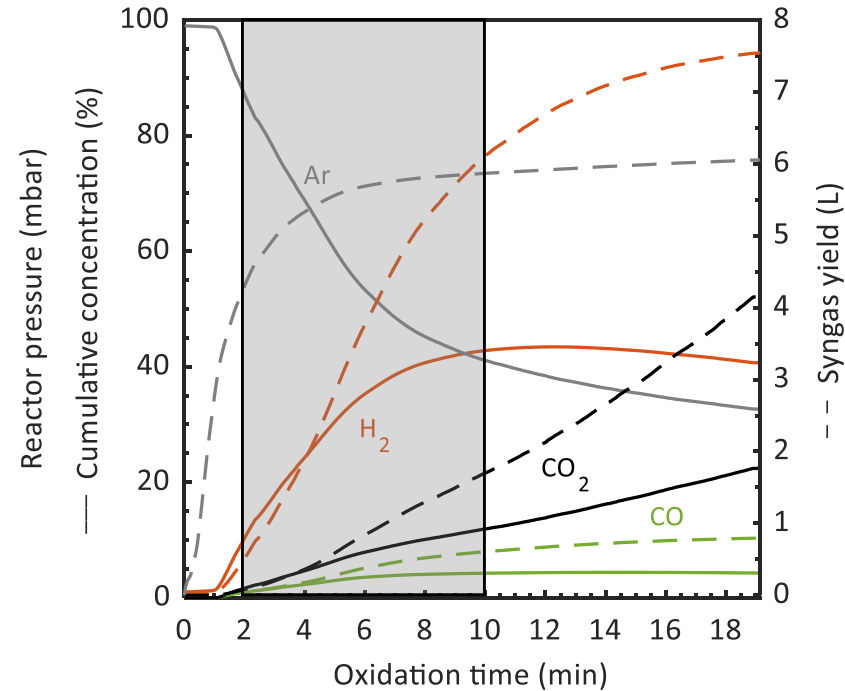
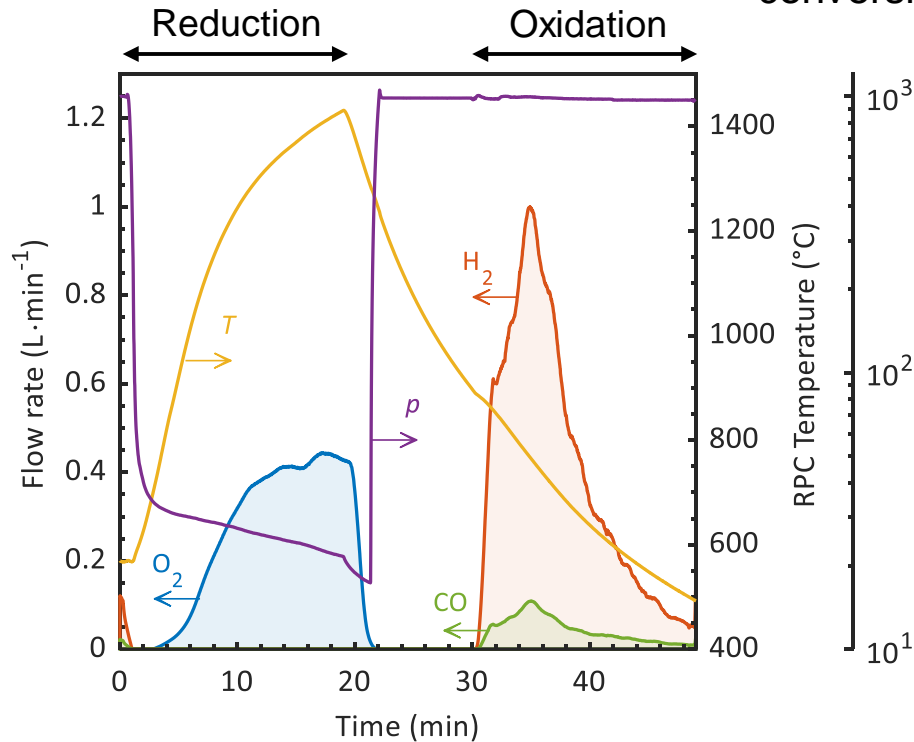
Conditions	Reduction	Oxidation
Power input	5.1 kW	Off-sun (0 kW)
Gas flow	0.5 l/min Ar	0.4 l/min CO_2 9.8 g/min H_2O
Pressure	25 mbar	1 bar

Exemplary Cycle Targeting Syngas for Methanol Synthesis

Target:

H_2/CO_x ratio: 2 – 3

Depending on catalyst and CO_2 conversion

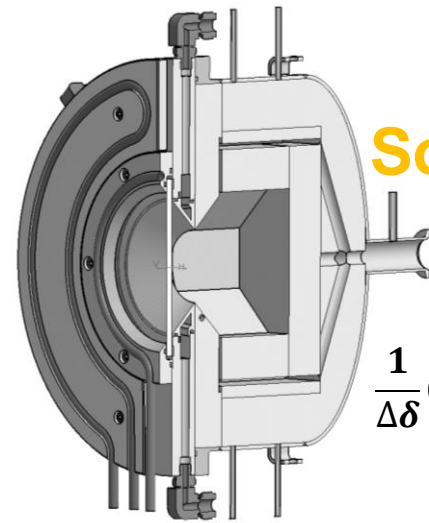
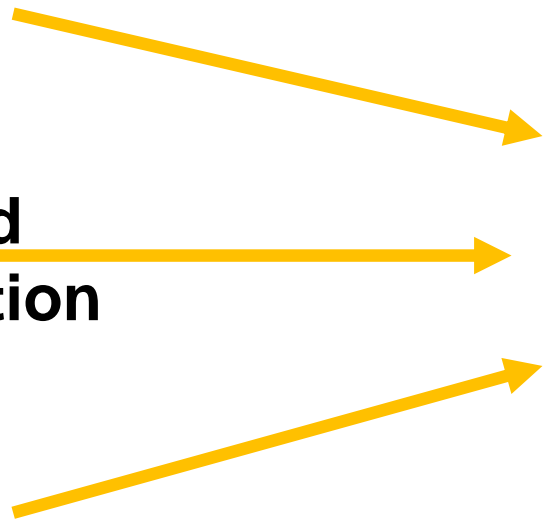


- Full oxidation:
 - 18.5 L of syngas
 - 40.7% H₂, 4.3% CO, 22.4% CO₂, 32.6% Ar
 - H₂/CO_x ratio: 1.52
 - CO₂ conversion: 16.1%
- Collection 2-10 min:
 - 9.4 L of syngas
 - 59.9% H₂, 6% CO, 17.2% CO₂, 16.9% Ar
 - H₂/CO_x ratio: 2.58
 - CO₂ conversion: 25.7%

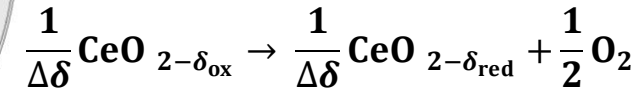
Conditions	Reduction	Oxidation
Power input	5.1 kW	Off-sun (0 kW)
Gas flow	0.5 l/min Ar	0.4 l/min CO ₂ 9.8 g/min H ₂ O
Pressure	25 mbar	1 bar

Parallel Operation of two Reactors

Concentrated
Solar Irradiation

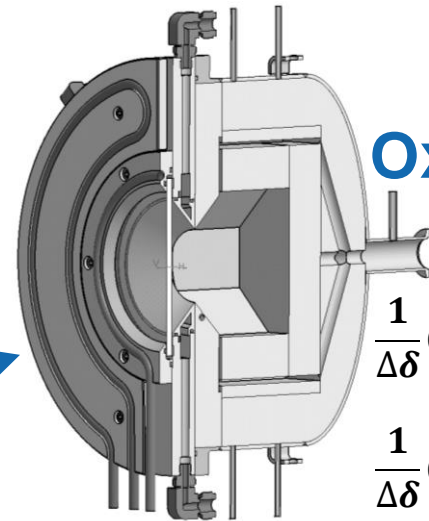


Solar Reduction

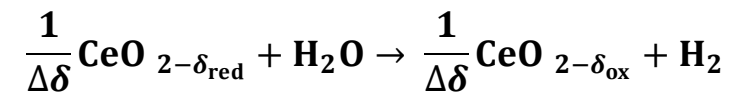
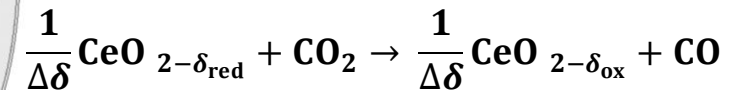


O₂

CO₂ / H₂O



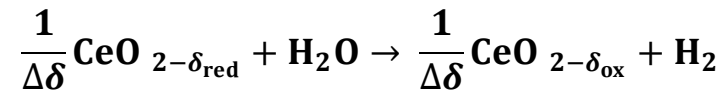
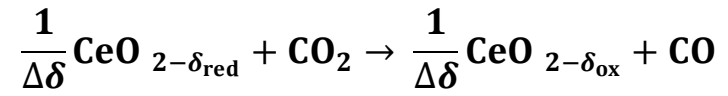
Oxidation



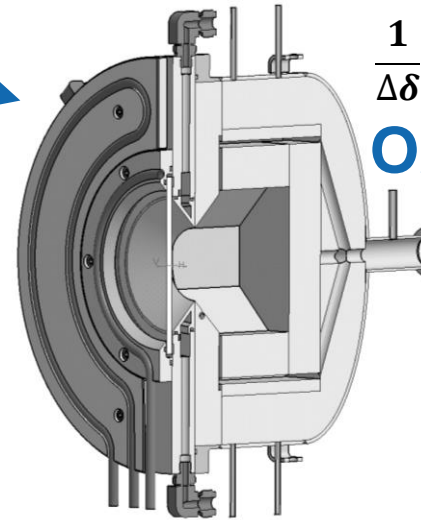
CO / H₂

Parallel Operation of two Reactors

CO₂ / H₂O



Oxidation

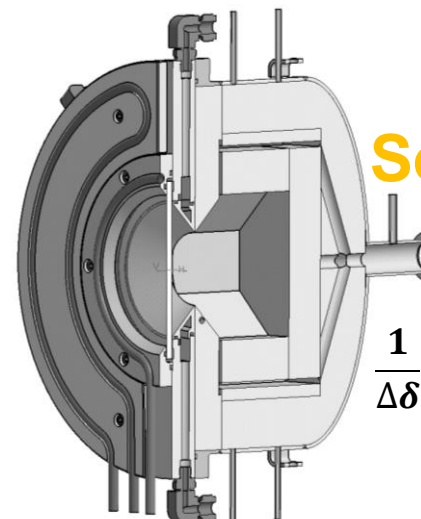
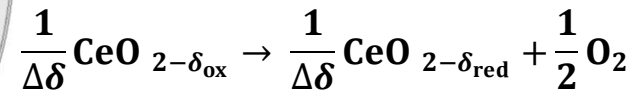


O₂

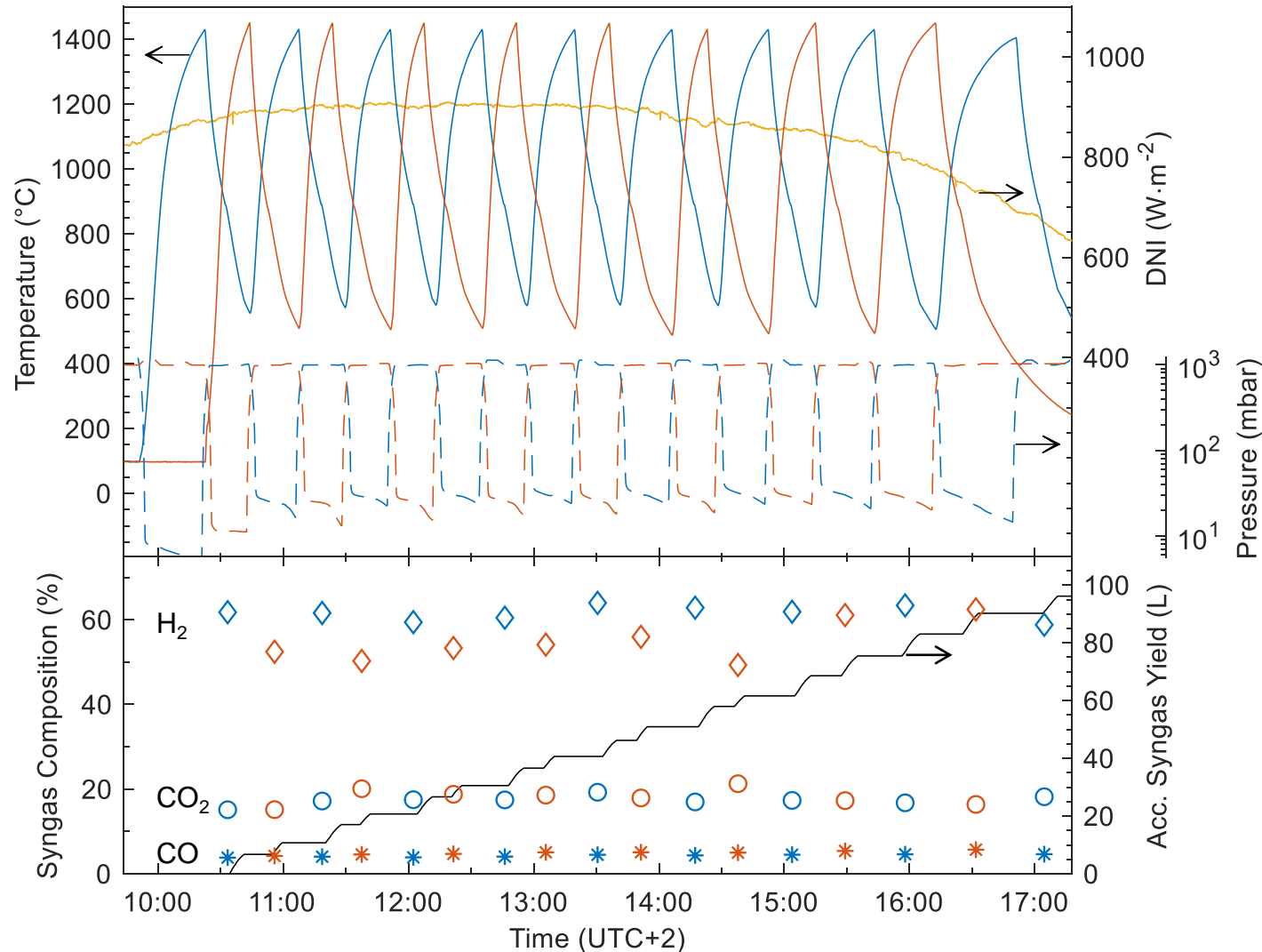
CO / H₂

Concentrated
Solar Irradiation

Solar Reduction



Exemplary Day Targeting Syngas for Methanol Synthesis



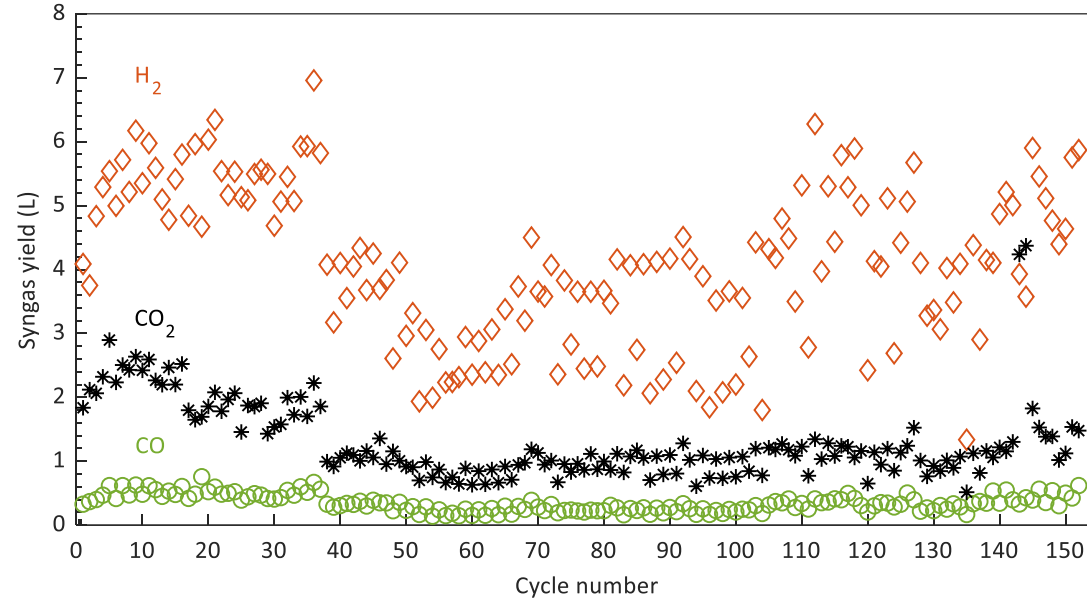
- 17 cycles:
 - 96.2 L of syngas
 - 57.2% H₂, 4.4% CO, 16.8% CO₂, 17.7% Ar
 - H₂/CO_x ratio: 2.7
 - CO₂ conversion: 21%

- **Increase $\eta_{solar-to-fuel}$:**

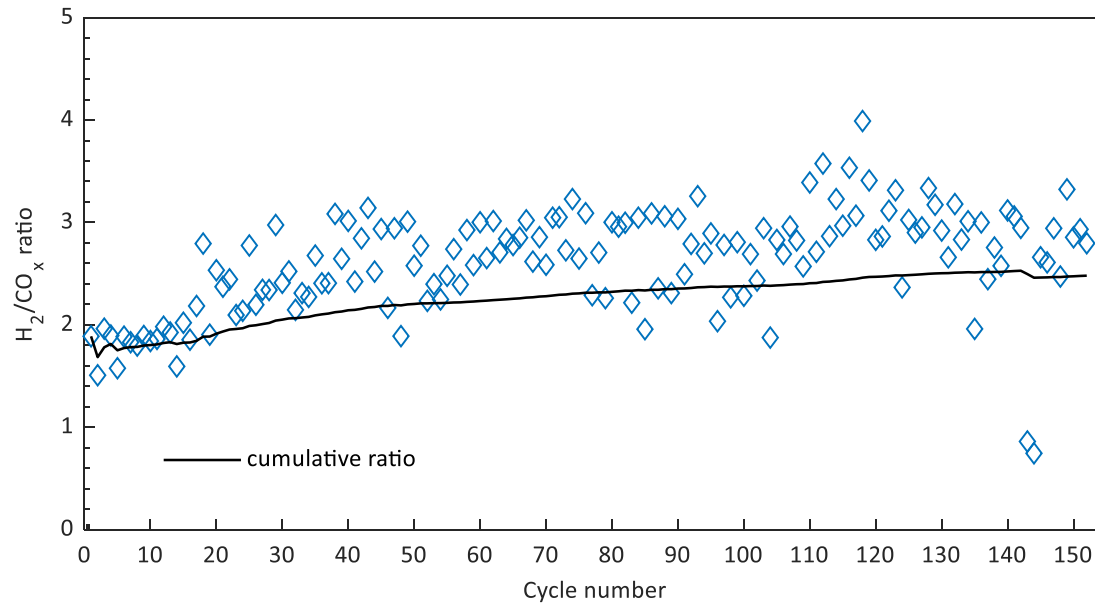
- $$\eta_{solar-to-fuel} = \frac{Q_{fuel}}{Q_{solar} + Q_{inert} + Q_{pump}} = 1.9 - 3.8\% \quad (5.6\% \text{ on solar tower})$$

- Optimize operation parameters/setup
- Optimise porous ceramic structure (all participating)
- Heat recovery (T-swing)

Production Campaign Targeting Syngas for Methanol Synthesis



- 152 cycles:
 - 1069.7 L of syngas
 - 58.4% H₂, 5% CO, 18.6% CO₂, 18% Ar
 - H₂/CO_x ratio: 2.48
 - CO₂ conversion: 21%



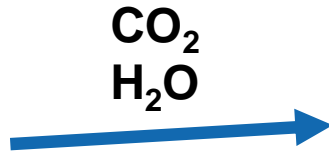
Source: Schäppi, R. *et al.* Drop-in Fuels from Sunlight and Air. *Nature* (2021).

Efficiency of the implemented process chain



Direct Air Capture Unit

$$\eta_{\text{DAC}} \approx 90\%$$

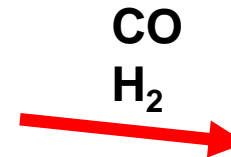


Solar Redox Unit

$$\eta_{\text{optical}} = 59.6\%$$

$$\eta_{\text{solar-to-syngas}} = 1.9 - 3.8\% \text{ (5.6\%)}$$

$$\eta_{\text{solar redox unit}} = \eta_{\text{optical}} \cdot \eta_{\text{solar-to-syngas}} = 1.1 - 2.3\%$$



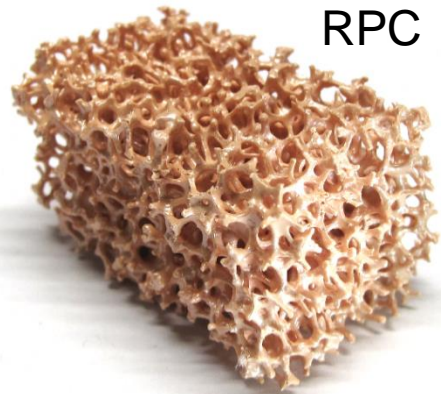
Gas-to-Liquid Synthesis Unit

$$\eta_{\text{GTL}} = 75\%$$

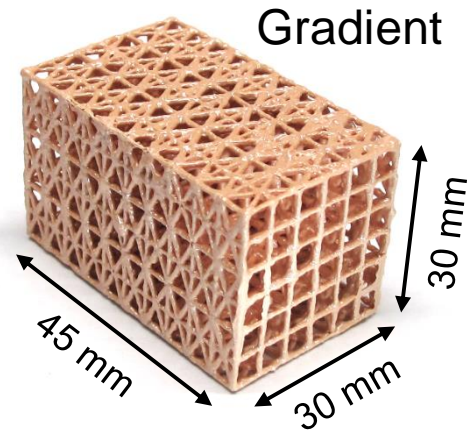
$$\eta_{\text{system}} = \eta_{\text{DAC}} \cdot \eta_{\text{solar redox unit}} \cdot \eta_{\text{GTL}} = \mathbf{0.8\%}$$

potential of exceeding $\eta_{\text{system}} = 13\%$

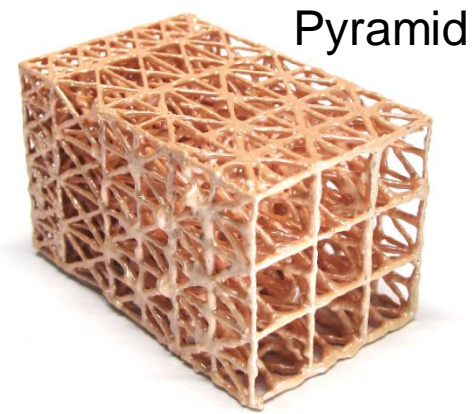
Research Projects to Optimise Ceramic Structures



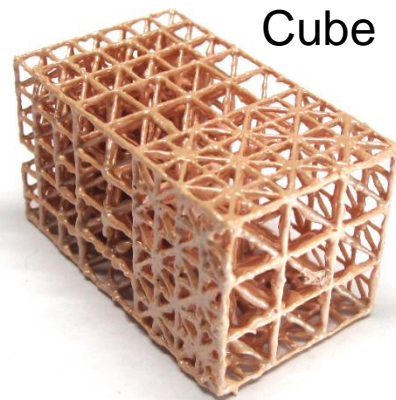
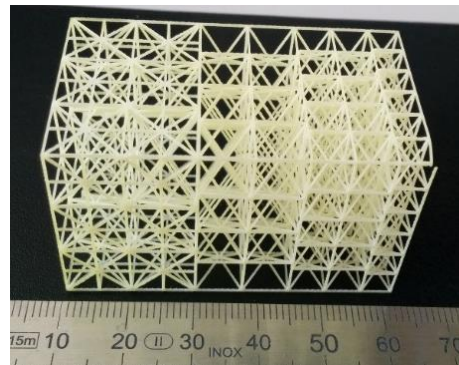
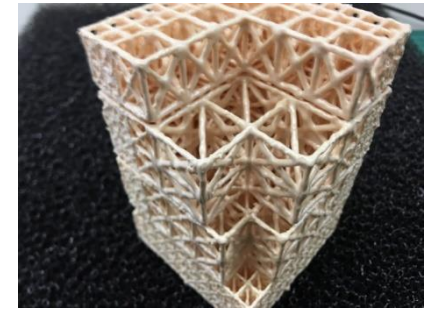
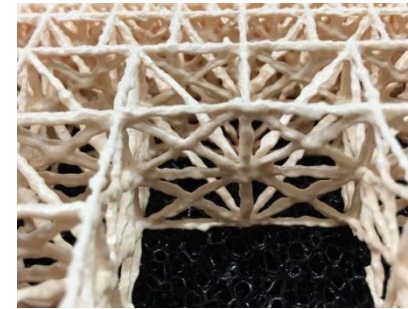
RPC



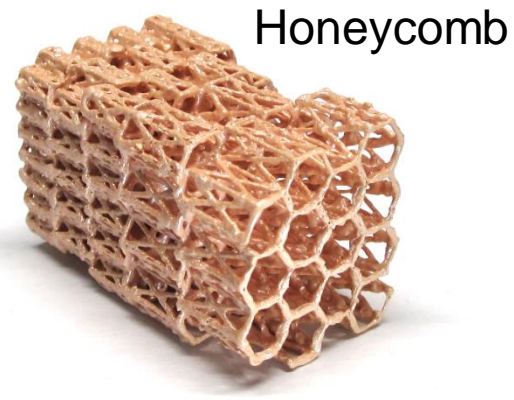
Gradient



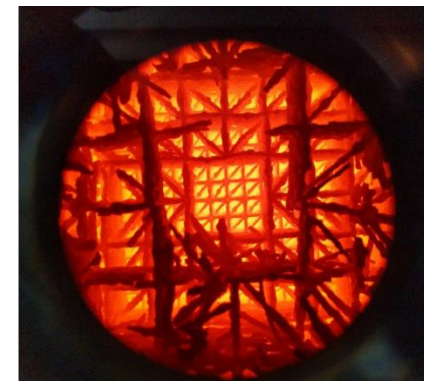
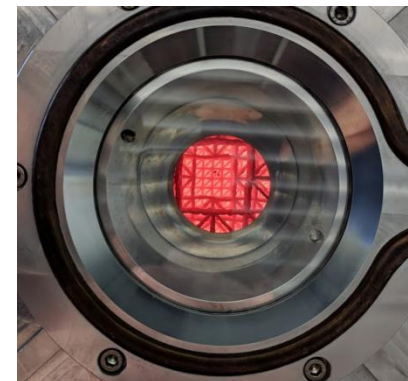
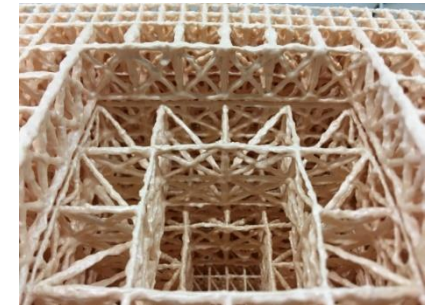
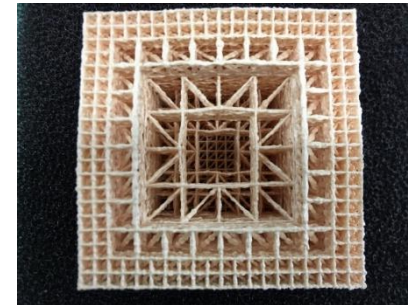
Pyramid



Cube

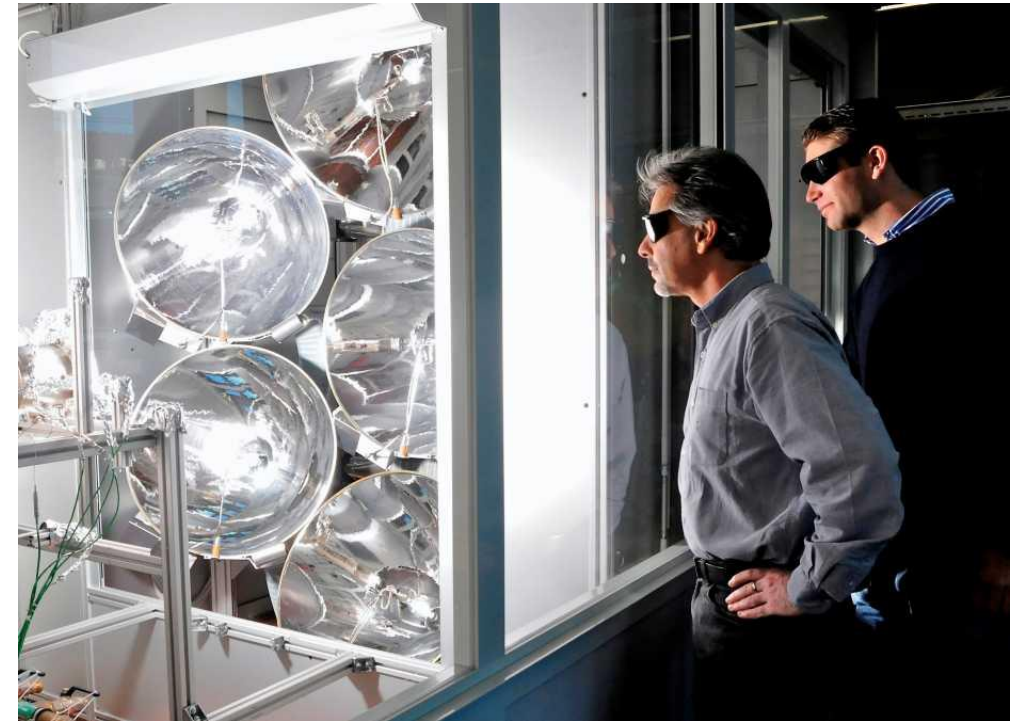
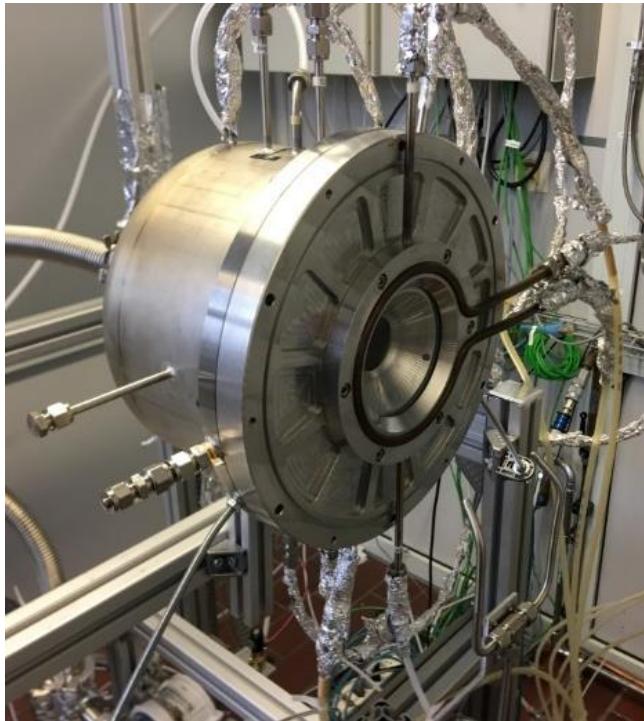


Honeycomb

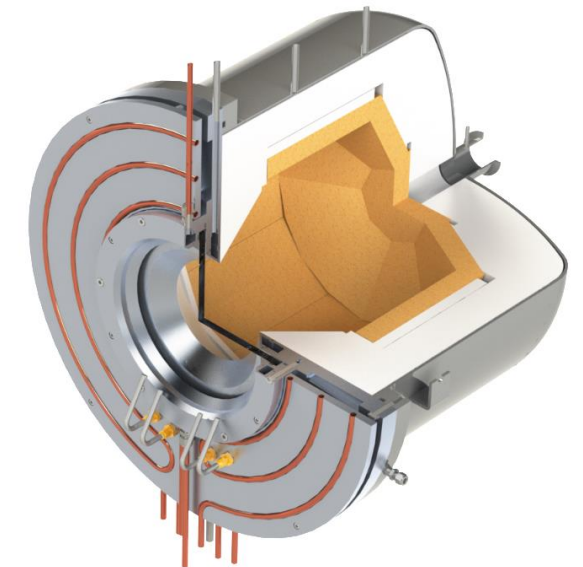
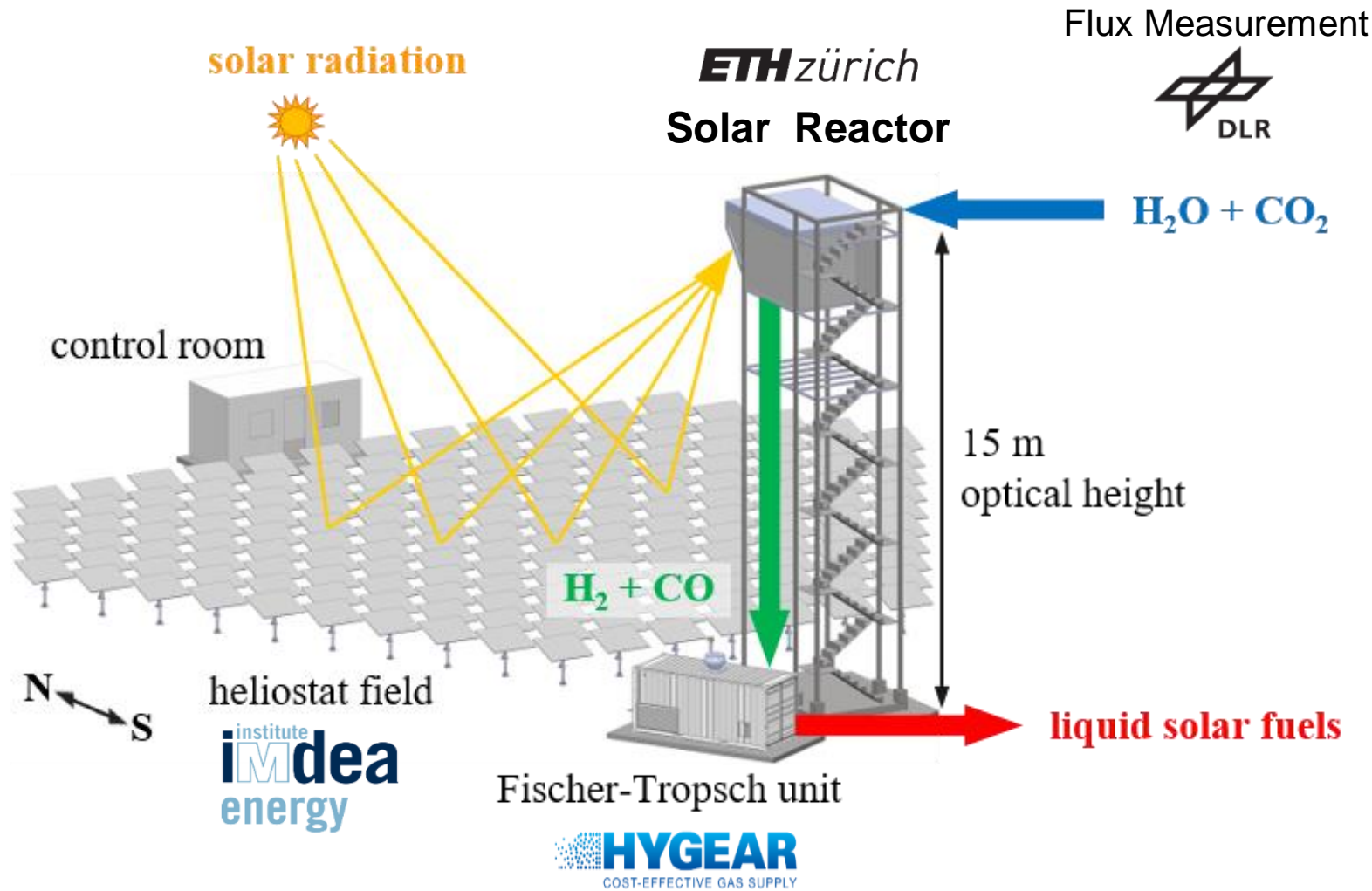


High-flux solar simulator

- Indoor test stand for solar reactors and installations



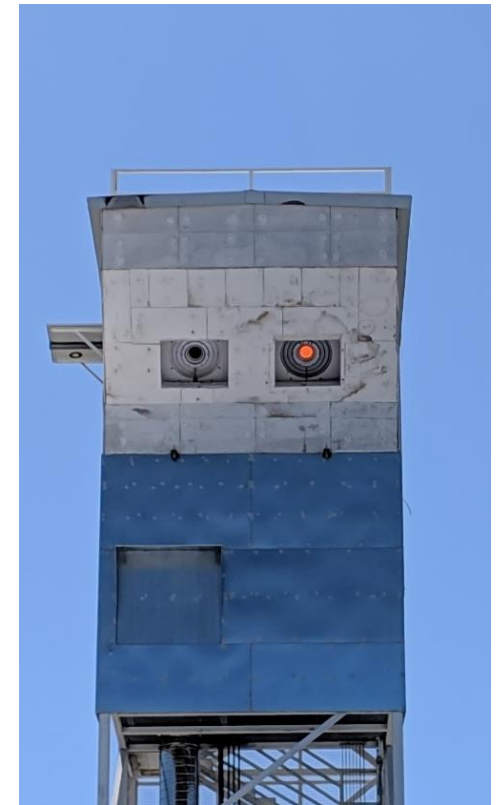
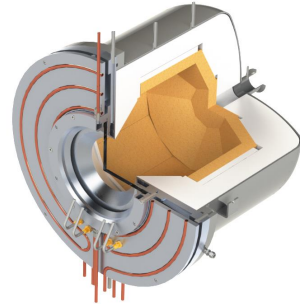
Sun-to-liquid Project (Móstoles, Spain)



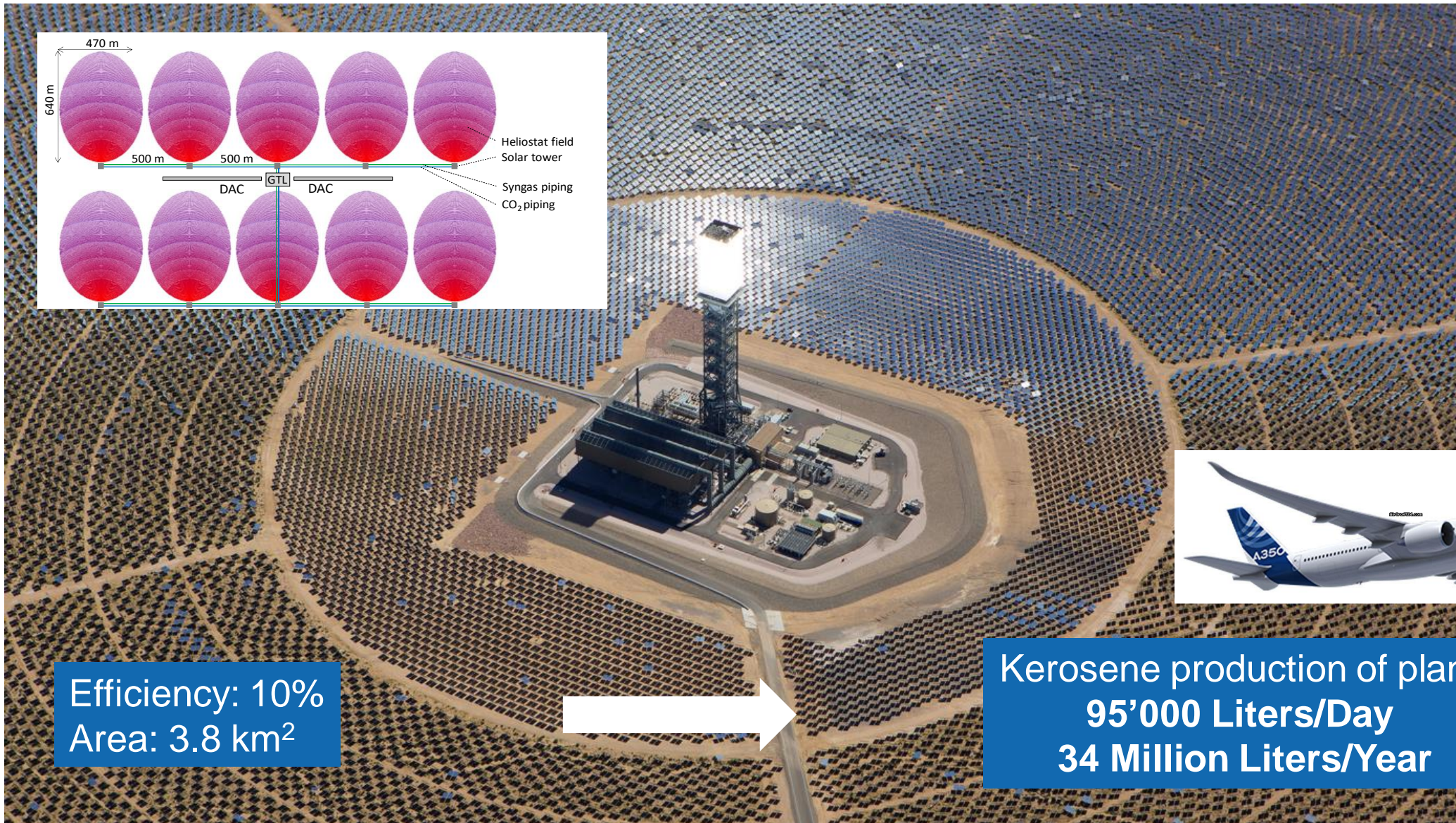
Generation 2
50 kW Pilot-scale
RPC

Sun-to-liquid Project (Móstoles, Spain)

- Upscaling: 50 kW reactor
- Tower with 169 heliostats



Industrial Production Example: 10 x 100MW

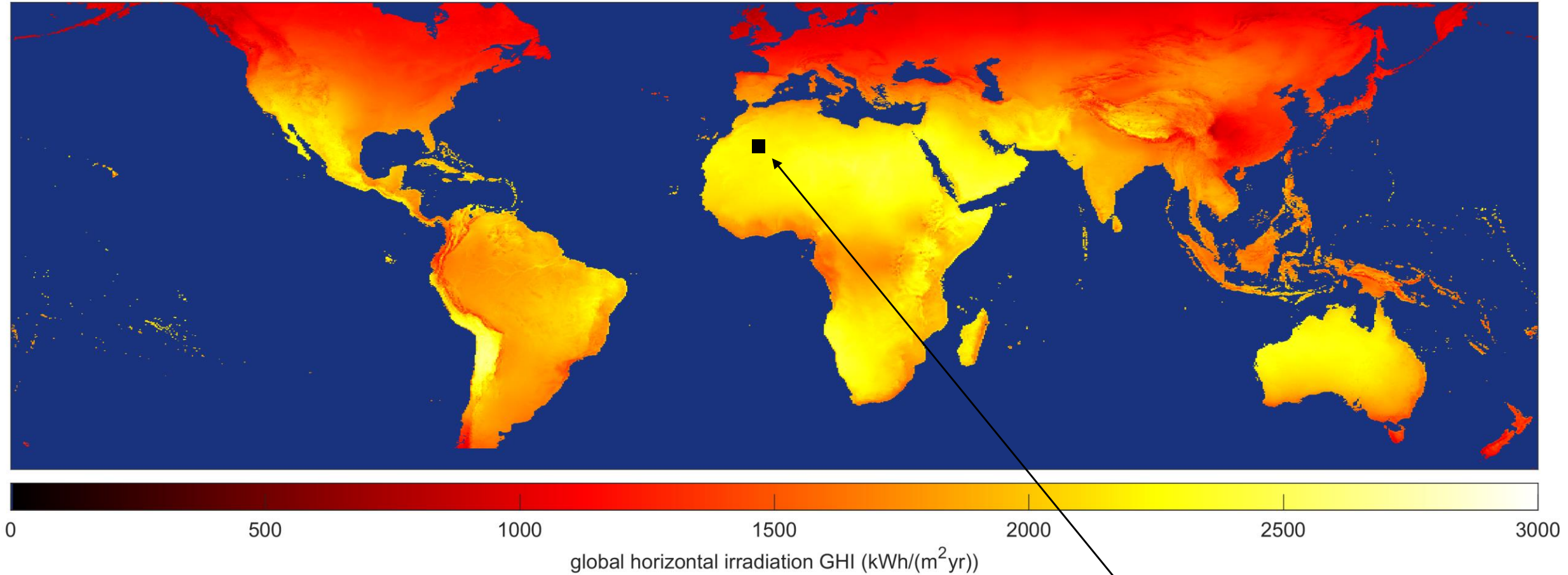


Efficiency: 10%
Area: 3.8 km²

Kerosene production of plant:
95'000 Liters/Day
34 Million Liters/Year



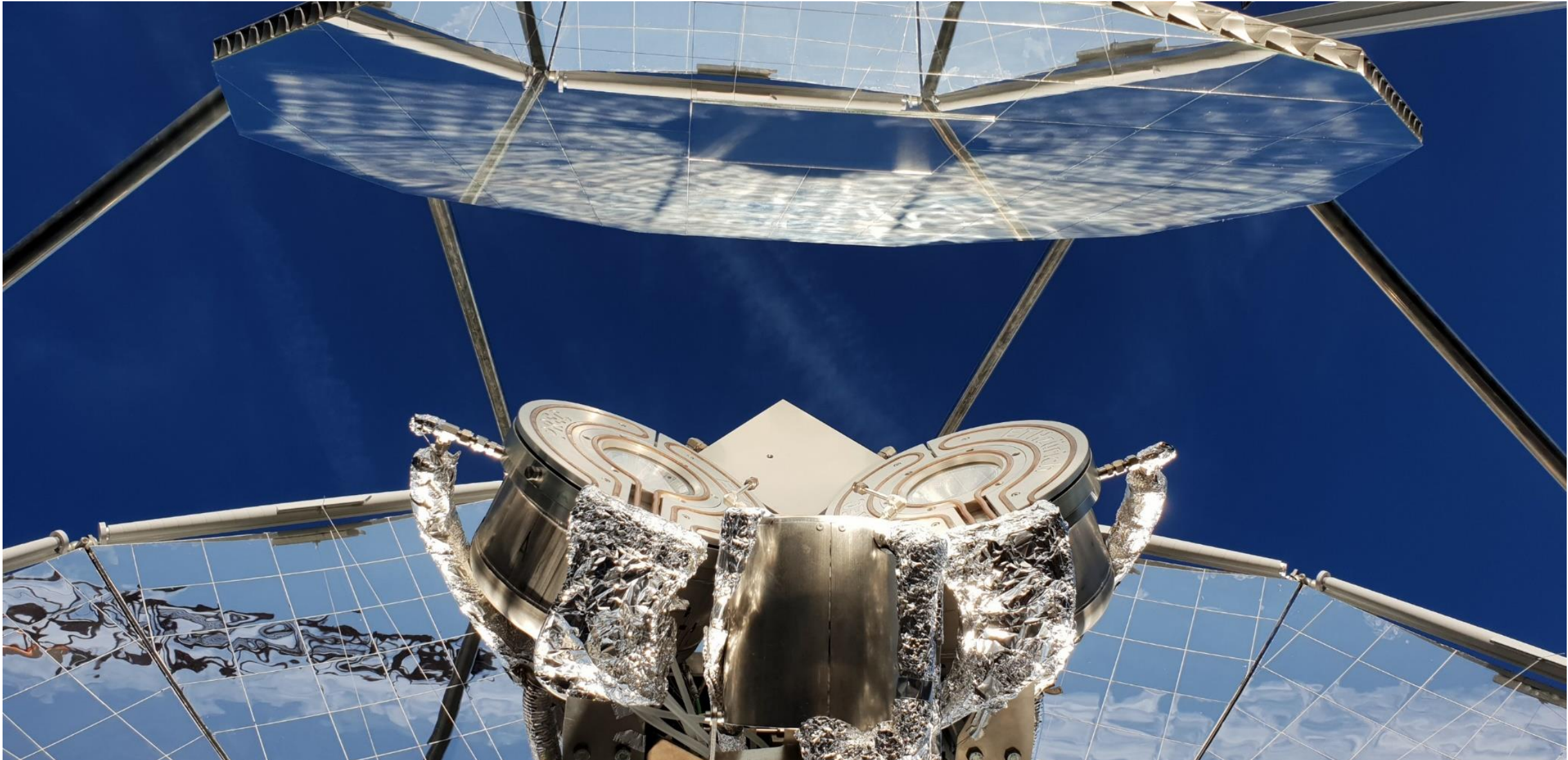
Where to build solar fuel plants?



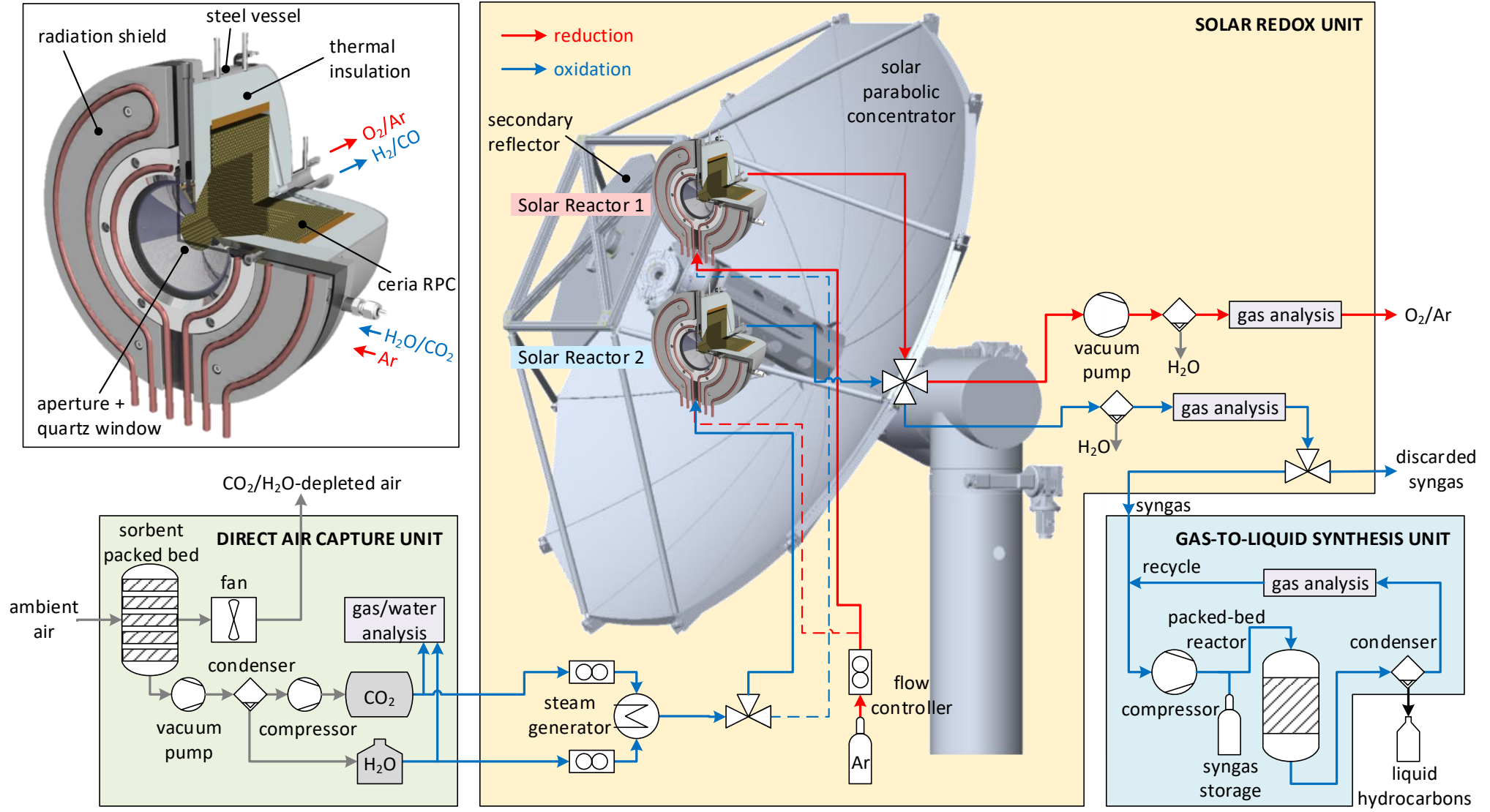
Global energy consumption traffic (2018): $2.890 \text{ Gtoe} = 3.3611 \cdot 10^{13} \text{ kWh}$
Yearly solar irradiation: 2000 kWh/m^2
Efficiency: 15%



Land requirements: $109'000 \text{ km}^2$
 $335 \times 335 \text{ km}$



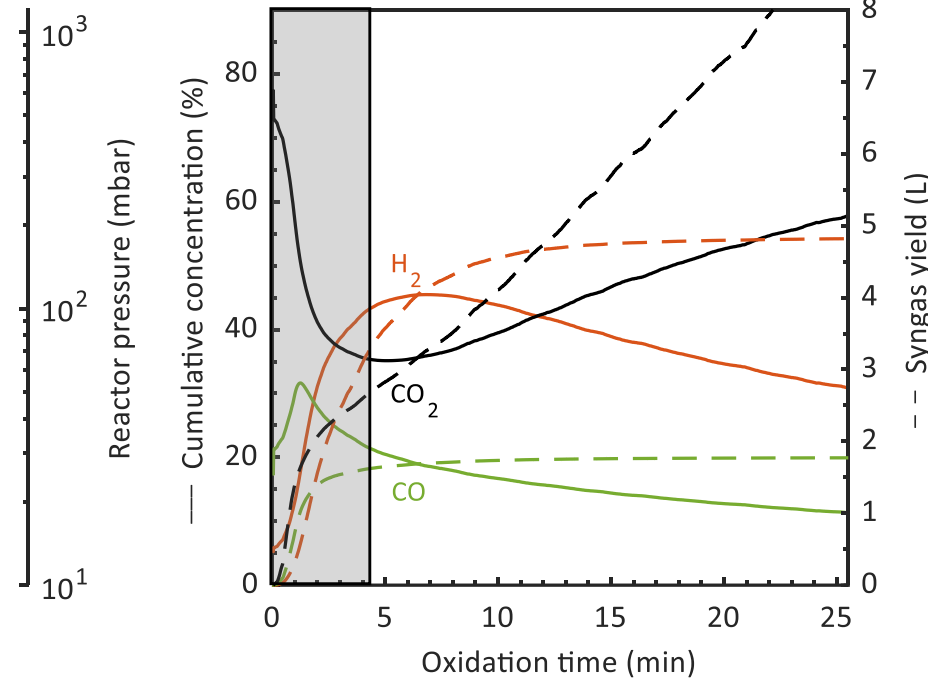
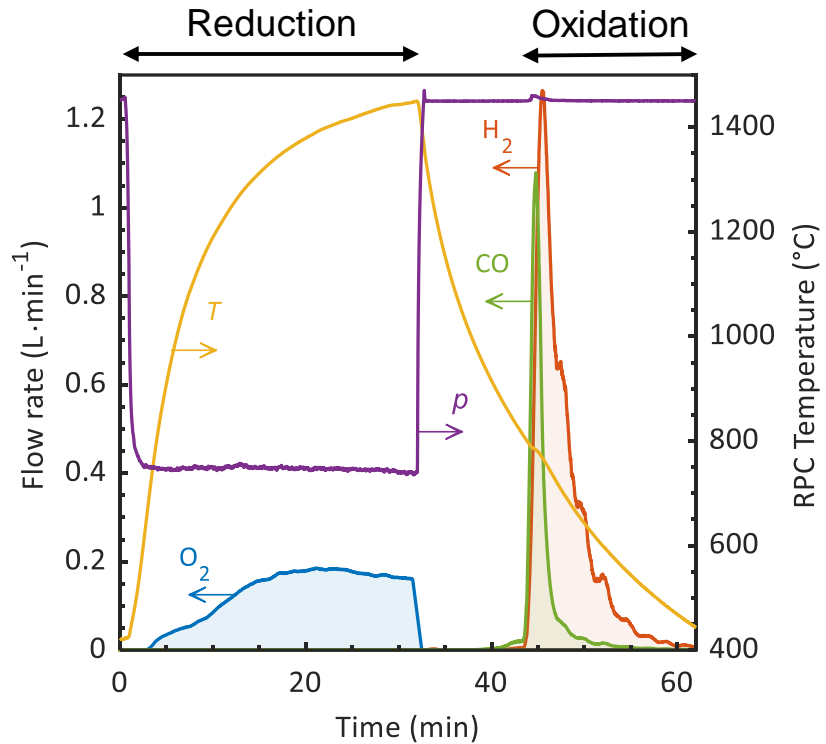
Schematic of the implemented process chain



Source: Schäppi, R. *et al.* Drop-in Fuels from Sunlight and Air. *Nature* (2021).

Exemplary Cycle Targeting Syngas for Fischer-Tropsch Synthesis

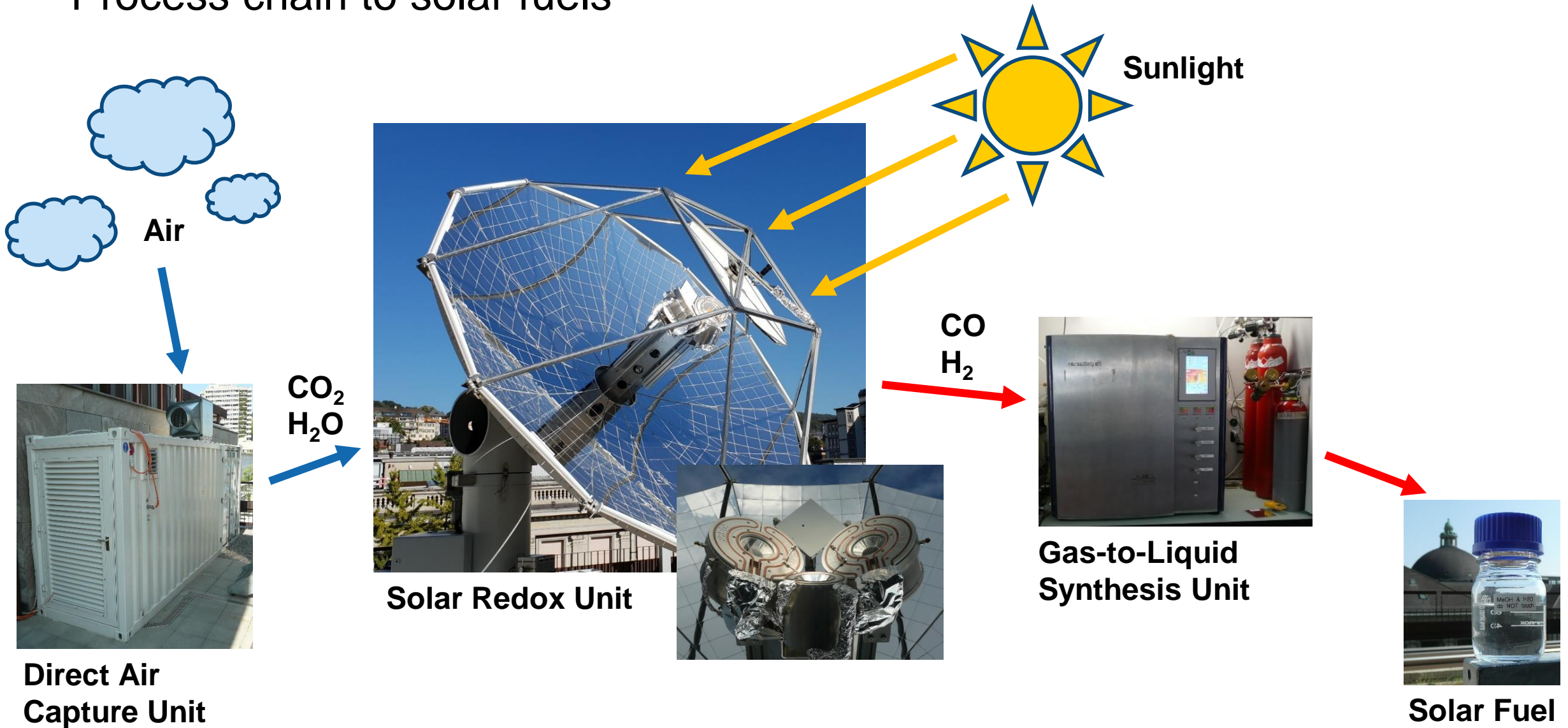
Target:
H₂/CO ratio: 2



- Full oxidation:
 - 15.6 L of syngas
 - 31.0% H₂, 11.4% CO, 57.6% CO₂
 - H₂/CO ratio: 2.72
 - CO₂ conversion: 16.5%
- Collection 0-4.25 min:
 - 7.52 L of syngas
 - 43.1% H₂, 21.5% CO, 35.4% CO₂
 - H₂/CO ratio: 2
 - CO₂ conversion: 37.9%

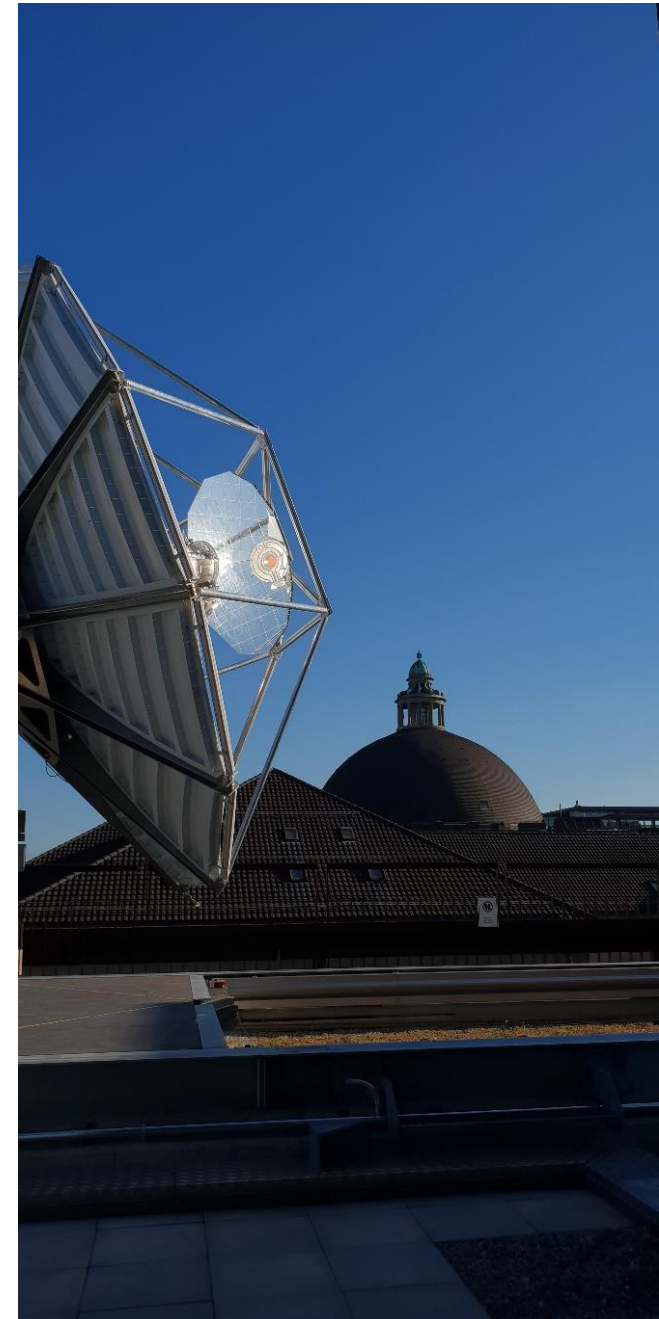
Conditions	Reduction	Oxidation
Power input	4.1 kW	Off-sun (0 kW)
Gas flow	0.5 l/min Ar	0.2 l/min CO ₂ 9.8 g/min H ₂ O
Pressure	50 mbar	1 bar

Process chain to solar fuels



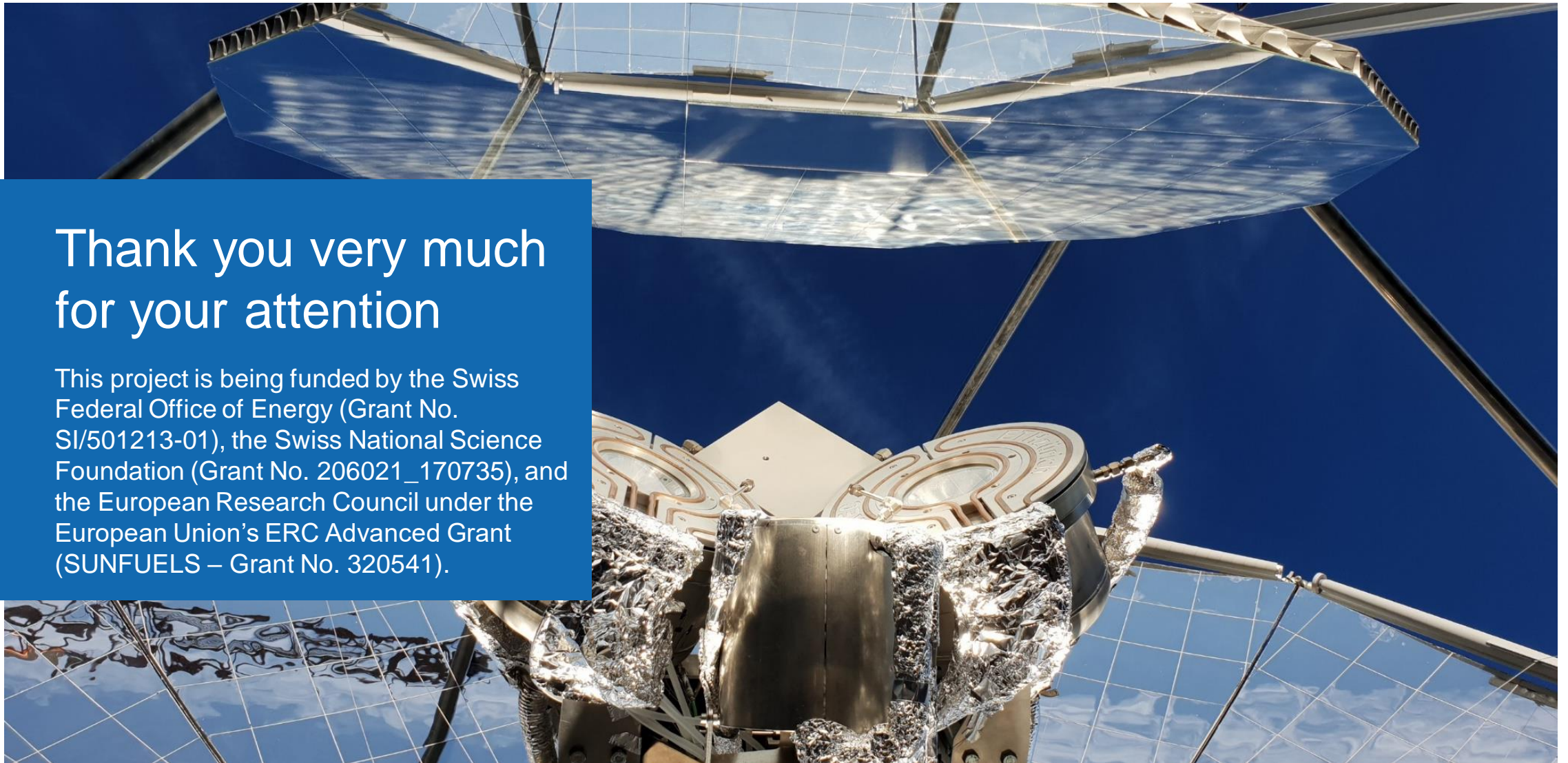
Conclusions

- Successful demonstration of the entire process chain from ambient air and sunlight to liquid solar fuels
- Syngas produced suitable for downstream methanol or Fischer-Tropsch synthesis
- Stable fully automated full day consecutive cycling
- Produced methanol and kerosene from sunlight and air
- Schäppi, R., Rutz, D., Dähler, F., Muroyama A., Haueter P., Lilliestam J., Patt A., Furler P., Steinfeld A., **Drop-in Fuels from Sunlight and Air**. *Nature* (2021).



Thank you very much for your attention

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